



U.S. DEPARTMENT OF  
**ENERGY**

Energy Efficiency &  
Renewable Energy



# Notice of Proposed Rulemakings for **Pumps** Test Procedure and Standards

April 29, 2015

**Ashley Armstrong**

Department of Energy

Building Technologies Program

EERE-2013-BT-TP-0055

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# Welcome

- Introductions (around the room)
- Role of the Facilitator
- Ground Rules
  - Speak one at a time.
  - Say your name for the record – there will be a complete transcript of this meeting.
  - Be concise – share the ‘air-time’.
  - Keep the focus here – cell phones on silent; limit sidebar conversations.
  - Webinar participants turn phone on mute; “raise your hand” to be recognized to speak.
- Housekeeping Items
- Agenda Review
- Opening Remarks

# Agenda – Morning (TP)

- 1) 9:00 AM Introductions & Stakeholder Opening Statements
- 2) 9:30 AM Regulatory History & Scope
- 3) 10:00 AM Metric
- 4) 10:30 AM Test Procedure: Determination of Pump Performance
- 5) 11:00 AM Break
- 6) 11:15 AM Test Procedure: Determination of Driver Efficiency
- 7) 11:45 AM Test Procedure: Calculation & Testing Based Methods
- 8) 12:30 PM Test Procedure: Sampling Plan
- 9) 12:45 PM Test Procedure: Burden
- 10) 1:00 PM Lunch

# Agenda – Afternoon (ECS)

- 1) 2:00 PM Welcome, Introductions, Opening Statements
- 2) 2:10 PM Overview, Scope, Market and Technology Assessment, Screening Analysis
- 3) 2:30 PM Engineering Analysis
- 4) 3:00 PM Energy Use, Markup Analysis, Life-Cycle Cost and Payback Period Analysis
- 5) 3:40 PM Break
- 6) 3:50 PM Shipments, National Impact Analysis
- 7) 4:20 PM Manufacturer Impact Analysis
- 8) 4:35 PM Utility Impact Analysis, Employment Impact Analysis, Emissions Analysis, Regulatory Impact Analysis
- 9) 4:45 PM Closing Remarks

# Public Meeting Slides Topics – Morning (TP)

- 1 Introductions & Stakeholder Opening Statements
- 2 Regulatory History & Scope
- 3 Metric
- 4 Test Procedure: Determination of Pump Performance
- 5 Break
- 6 Test Procedure: Determination of Driver Efficiency
- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Public Meeting Slide Topics – Afternoon (ECS)

- 1 Overview
- 2 Market & Technology; Screening
- 3 Engineering
- 4 Markups Analysis; Energy Use
- 5 Life-Cycle Cost & Payback Period Analysis
- 6 Shipments; National Impact Analysis
- 7 MIA; NOPR Analyses; Closing Remarks
- 8 Proposed Standards; Labeling and Certification; Closing Remarks

# Listening Via the Webcast

- DOE is broadcasting this meeting live over the Internet.
- DOE is providing the webcast to accommodate stakeholders who are unable to attend the public meeting in person.
- The web broadcast allows stakeholders to listen in and view the slides.
- All stakeholders are encouraged to submit written comments after the public meeting.

# Purpose of the Public Meeting

- Present DOE's proposed test procedure and energy conservation standards for pumps.
  - Morning = Test Procedure Notice of Proposed Rulemaking (NOPR)
  - Afternoon = Energy Conservation Standards NOPR
- Discuss next steps in the rulemakings.
- Invite comment on:
  - the test procedure NOPR;
  - the energy conservation standard NOPR; and
  - any additional issues raised by interested parties.



# Opening Remarks

Meeting participants are invited to provide opening remarks or statements at this time.

# Issues for Discussion

- DOE welcomes comments, data, and information concerning its proposed test procedure and energy conservation standards for pumps. Whether invited by an issue box or not, comments are welcome on any part of DOE's analysis.

**Issue Box:** Issue boxes in the test procedure section of this presentation correspond to the list of issues published at the end of the NOPR document. These issues will be numbered corresponding to the numbers presented in section V.E of the pumps test procedure NOPR.

- Issue boxes are not included for the energy conservation standard section of this presentation, as the analysis was discussed with the Working Group and directly supports their Recommendations.

# How to Submit Written Comments

In all correspondence, please refer to these pumps rulemakings by:

<u>Title</u>	<b>Pumps Test Procedure</b>	<b>Pumps Energy Conservation Standard</b>
<u>Docket Number:</u>	<a href="#">EERE-2013-BT-TP-0055</a>	<a href="#">EERE-2011-BT-STD-0031</a>
<u>Regulation Identification Number (RIN):</u>	1904-AD50	1904-AC54
<u>Email:</u>	<a href="mailto:Pumps2013TP0055@ee.doe.gov">Pumps2013TP0055@ee.doe.gov</a>	<a href="mailto:Pumps2011STD0031@ee.doe.gov">Pumps2011STD0031@ee.doe.gov</a>
<u>Comments Due:</u>	June 15, 2015, 11:59 PM ET	June 1, 2015, 11:59 PM ET

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# Statutory Authority

- The Energy Policy and Conservation Act (EPCA) of 1975 established an energy conservation program for certain commercial and industrial equipment.
  - This program includes pumps as covered equipment. (42 U.S.C. 6311(1)(A))
  - EPCA authorizes DOE to issue standards, test procedures, and labeling requirements for covered equipment. (42 U.S.C. 6295(r), 42 U.S.C. 6315(a), 42 U.S.C. 6316(a)(1))
- Manufacturers must use the test procedure as the basis for:
  - Certifying to DOE that their equipment complies with applicable energy conservation standards adopted under EPCA. (42 U.S.C. 6295(s) and 6316(a)(1)), and
  - Making representations about the energy consumption of the equipment. (42 U.S.C. 6314(d))

# Regulatory History: Pumps

- There are currently no Federal energy conservation standards or test procedures for pumps.
- On June 13, 2011, DOE issued a Request for Information (RFI) to gather information related to pumps. 76 FR 34192.
- On February 1, 2013, DOE published a Framework document discussing potential methodologies for considering new energy conservation standards and a new test procedure for pumps. 78 FR 7304.
- On July 23, 2013, DOE issued a notice of intent to form a Working Group under the Appliance Standards Rulemaking Federal Advisory Committee (ASRAC) to negotiate energy conservation standards for pumps (Commercial and Industrial Pumps [Pumps] Working Group). 78 FR 44036.

# Pumps Working Group Membership

- The members of the Pumps Working Group were selected to ensure a broad and balanced representation of stakeholder interests.

Member	Affiliation
Lucas Adin	U.S. Department of Energy
Tom Eckman	Northwest Power and Conservation Council (ASRAC Member)
Robert Barbour	TACO, Inc.
Charles Cappelino	ITT Industrial Process
Greg Case	Pump Design, Development and Diagnostics
Gary Fernstrom	Pacific Gas & Electric Company, San Diego Gas & Electric Company, Southern California Edison, and Southern California Gas Company
Mark Handzel	Xylem Corporation
Albert Huber	Patterson Pump Company
Joanna Mauer	Appliance Standards Awareness Project
Doug Potts	American Water
Charles Powers	Flowserve Corporation, Industrial Pumps
Howard Richardson	Regal Beloit
Steve Rosenstock	Edison Electric Institute
Louis Starr	Northwest Energy Efficiency Alliance
Greg Towsley	Grundfos USA
Meg Waltner	Natural Resources Defense Council

# Regulatory History: Pumps Working Group

- Between December 2013 and June 2014, DOE held seven open meetings and two webinars to discuss scope, metrics, test procedures, and standard levels for pumps.
  - Details of the negotiation sessions and related materials can be found in the docket for the Working Group (<http://www.regulations.gov/#!docketDetail;D=EERE-2013-BT-NOC-0039>).
- The Pumps Working Group concluded on June 19, 2014, producing 14 recommendations for DOE related to pump energy conservation standards and the pump test procedure (Working Group Recommendations).
  - ASRAC voted unanimously to approve the Working Group Recommendations during a July 7, 2014 webinar.
- DOE's proposed pumps test procedure reflects the Working Group Recommendations.
  - Additional details are discussed in this presentation.
- DOE's proposed energy conservation standards directly reflect the Working Group Recommendations.



# Pumps Test Procedure Rulemaking

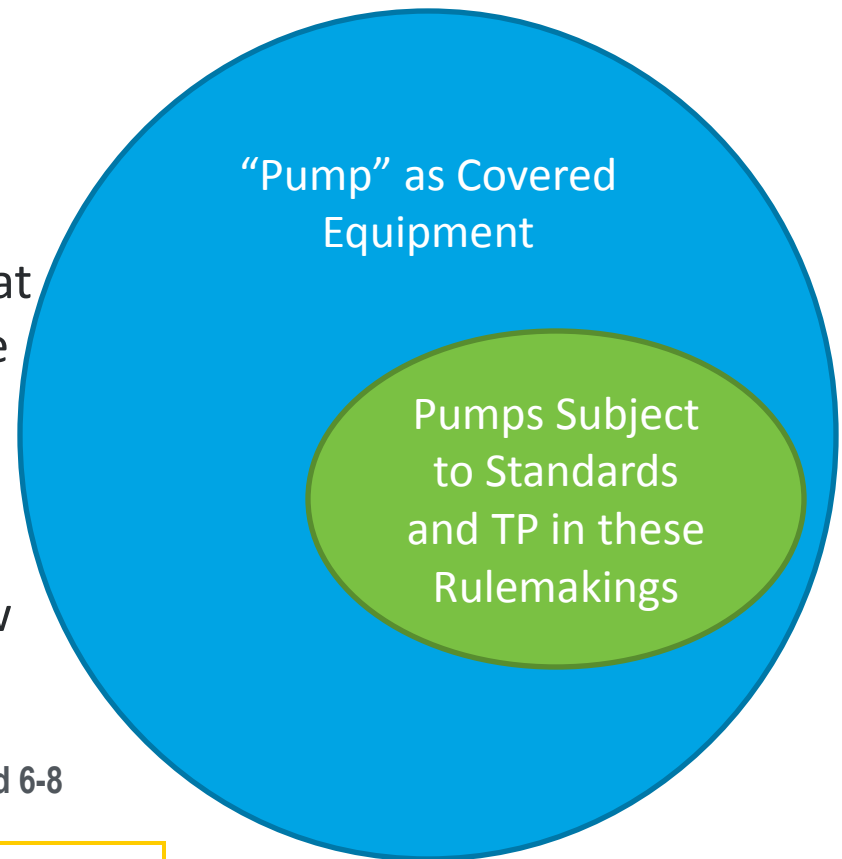


- NOPR issued by DOE on March 13, 2015
  - NOPR published in the Federal Register on April 1, 2015 (80 FR 17586)
  - NOPR Public Meeting today, April 29, 2015
- Comments on NOPR from interested parties accepted until **June 15, 2015**.
  - DOE reviews and considers all written and oral comments
    - Transcript records oral comments from today’s public meeting
    - Written comments
- Final Rule is expected to be issued by December 2015.

# Scope of Covered Equipment

- “Pump” is listed as a type of covered equipment under EPCA, but is not defined.
- Defining “pump” characterizes the overall scope of coverage for pumps that can be considered in current and future rulemakings.
- The proposed energy conservation standards and test procedure are limited to an identical and more narrow range of equipment.

Pumps Working Group Recommendation # 4 and 6-8

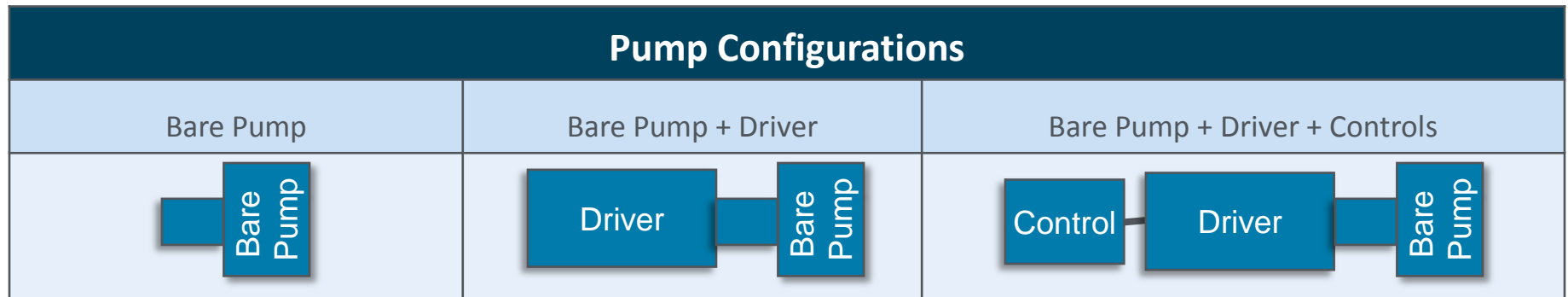


**Issue 1:** DOE requests comment on its proposal to match the scopes of the pump test procedure and energy conservation standard rulemakings, as recommended by the Working Group.

# Proposed Definition of Pump

- **Pump** means equipment **that is designed** to move liquids (which may include entrained gases, free solids, and totally dissolved solids) by physical or mechanical action, and includes a bare pump and, if included by the manufacturer **at the time of sale**, mechanical equipment, driver, and controls.

Pumps Working Group Recommendation # 1 (**with slight modification**)



# Proposed Definitions of Pumps Components

- DOE is also proposing definitions related to the components that comprise a pump, as recommended by the Working Group:
  - **Bare pump** means a pump excluding mechanical equipment, driver, and controls.
  - **Mechanical equipment** means any component of a pump that transfers energy from a driver to the bare pump.
  - **Driver** means the machine providing mechanical input to drive a bare pump directly or through the use of mechanical equipment. Examples include, but are not limited to, an electric motor, internal combustion engine, or gas/steam turbine.
  - **Control** means any device that can be used to operate the driver. Examples include, but are not limited to, continuous or non-continuous speed controls, schedule-based controls, on/off switches, and float switches.

Pumps Working Group Recommendation # 2 (with slight modification)

**Issue 2:** DOE requests comment on the proposed definitions for “pump,” “bare pump,” “mechanical equipment,” “driver,” and “control.”

# Proposed Pump-Specific Definition of a Basic Model

- DOE proposes the following pump-specific definition for basic model:
  - **Basic model** means all units of a given type of covered equipment (or class thereof) manufactured by one manufacturer, having the same primary energy source, and having essentially identical electrical, physical, and functional (or hydraulic) characteristics that affect energy consumption, energy efficiency, water consumption, or water efficiency; except that:
    - RSV\* and VTS\*\* pump models for which the bare pump differs in the number of stages must be considered a single basic model, and
    - pump models for which the bare pump differs in impeller diameter, or impeller trim, may be considered a single basic model or separate basic models.
- The certified ratings for a given pump basic model will be based on the specified numbers of stages required for testing under the test procedure and on that model's full impeller diameter.
  - Variations in motor sizing as a result of different impeller trims would not be a basis for differentiating basic models.

Pumps Working Group Recommendations # 7, 14

\* RSV = Radially split, multi-stage, vertical, in-line diffuser casing pump

\*\* VTS = Vertical turbine submersible pump

# Proposed Definition of Full Impeller



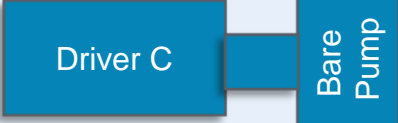
- DOE proposes a definition of full impeller that would:
  - apply to all pump models, including custom pumps and those that are only distributed in commerce with trimmed impellers, and
  - allow manufacturers the flexibility to rate a model with a trimmed impeller as less consumptive than at full impeller, if desired.
- **Full impeller diameter** means [*either*]:
  - (1) the maximum diameter impeller used with a given pump basic model distributed in commerce or
  - (2) the maximum diameter impeller referenced in the manufacturer’s literature for that pump basic model,whichever is larger.

Pumps Working Group Recommendations # 7 (with slight modification)

**Issue 7:** DOE requests comment on the proposed definition for “full impeller.”

# Basic Model for Pumps Sold with Motors

- Manufacturers often pair a given bare pump with several different motors of varying performance characteristics.
- To rate these pump and motor combinations, manufacturers may:
  - rate each pairing of a bare pump at full impeller with a motor as a unique basic model, OR
  - group multiple motor pairings with the same bare pump at full impeller into a single basic model.

Pump and Motor Combinations	Driver Performance	Energy Rating	
		Multiple Basic Models	Single Basic Model
	Highest Efficiency	Highest Efficiency	Lowest Efficiency
	Middle Efficiency	Middle Efficiency	
	Lowest Efficiency	Lowest Efficiency	

# Requests for Comment

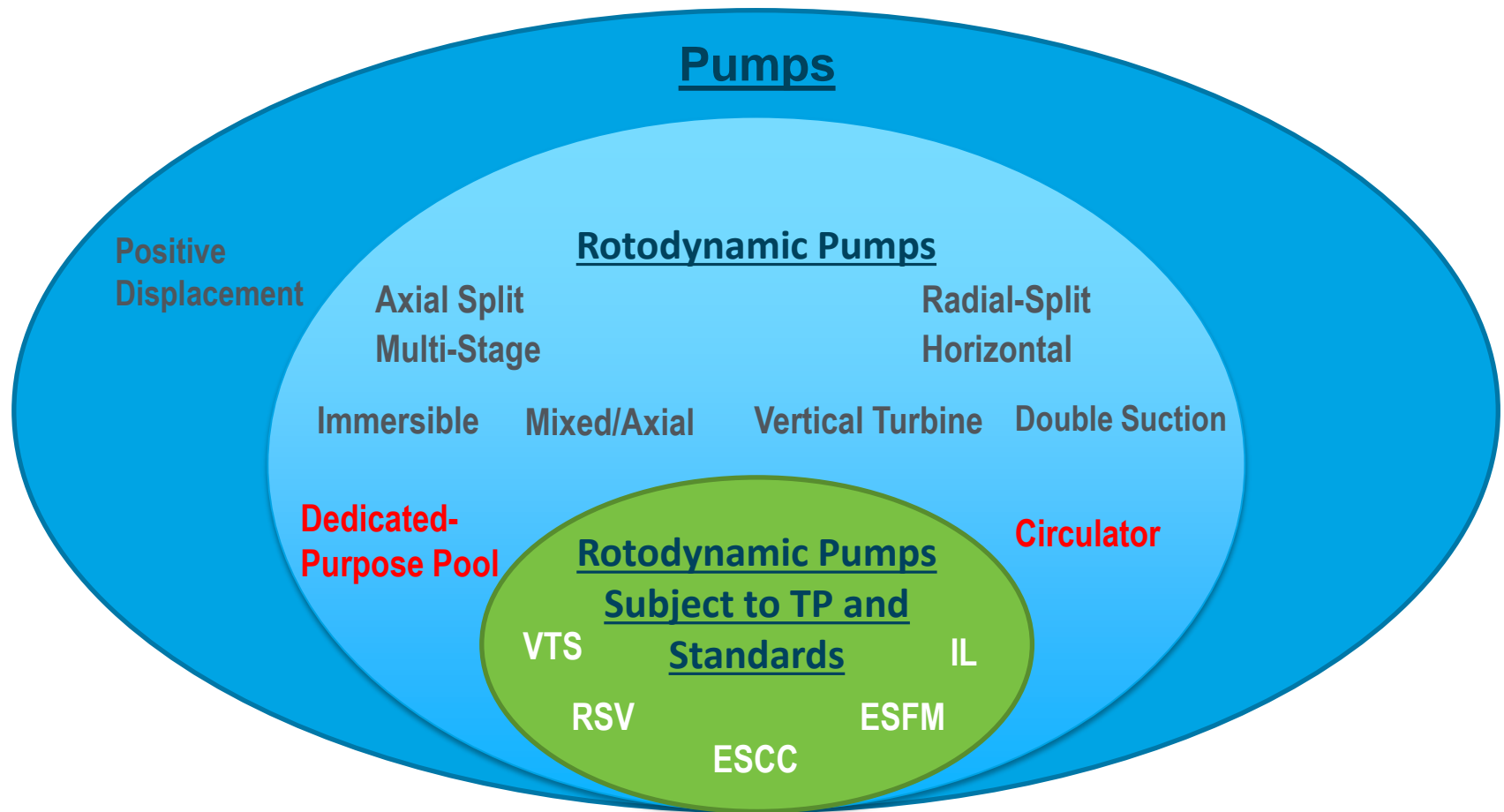
**Issue 6:** DOE requests comment on DOE's proposal to allow manufacturers the option of rating pumps with trimmed impellers as a single basic model or separate basic models, provided the rating for each pump model is based on the maximum impeller diameter available within that basic model.

**Issue 8:** DOE requests comment on the proposal to require that all pump models be rated in a full impeller configuration only.


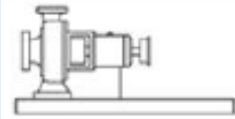





# Pump Categories

- DOE proposes that the test procedure and energy conservation standards are applicable to certain categories of rotodynamic pumps.



# Rotodynamic Pumps Subject to Proposed TP and Standards

	Equipment Class	Acronym	HI Nomenclature
 (A)	End Suction Close-Coupled	ESCC	OH7
 (A)	End Suction Frame Mounted	ESFM	OH0,OH1
 (A)	In-Line	IL	OH3, OH4, OH5
 (B)	Radially Split, Multi-Stage, Vertical, Inline Diffuser Casing	RSV	VS8
 (B)	Vertical Turbine Submersible	VTS	VS0

Note: Pump diagrams provided by HI.

Source: (A) 2014 version of ANSI/HI Standard 1.1-1.2, “Rotodynamic (Centrifugal) Pumps For Nomenclature And Definitions” (ANSI/HI 1.1-1.2–2014) or (B) 2008 version of ANSI/HI Standard 2.1-2.2, “Rotodynamic (Vertical) Pumps For Nomenclature And Definitions” (ANSI/HI 2.1-2.2–2008).

# Proposed Definitions of Pump Classes: Method

- DOE developed proposed definitions for the five pump equipment classes to accomplish the following:
  - Clearly identify the equipment that would be subject to the standards and test procedure.
    - DOE referenced HI nomenclature in the definitions as requested by stakeholders.
  - Create mutually exclusive equipment classes, e.g. ESCC versus ESFM.
  - Make the equipment classes mutually exclusive from other pumps not proposed to be part of this rulemaking, for example:
    - ESCC, ESFM, and IL versus circulators;
    - ESCC and ESFM versus dedicated-purpose pool pumps; and
    - RSV versus immersible pumps.
- DOE also proposed definitions for rotodynamic pump, end suction pump, and single axis flow pump to support the equipment class definitions.

## Add'l Proposed Definitions Related to Pump Equipment Classes

- **Rotodynamic pump** means a pump in which energy is continuously imparted to the pumped fluid by means of a rotating impeller, propeller, or rotor.
- **End suction pump** means a single-stage, **rotodynamic pump** in which the liquid enters the bare pump in a direction parallel to the impeller shaft and on the side opposite the bare pump's driver-end. The liquid is discharged through a volute in a plane perpendicular to the shaft.
- **Single axis flow pump** means a pump in which the liquid inlet of the bare pump is on the same axis as the liquid discharge of the bare pump.

# Proposed Definitions of Pump Equipment Classes (1)

- **End suction close-coupled (ESCC) pump** means an **end suction pump** in which:
  - (1) the motor shaft also serves as the impeller shaft for the bare pump;
  - (2) the pump requires attachment to a rigid foundation to function as designed and cannot function as designed when supported only by the supply and discharge piping to which it is connected; and
  - (3) the pump does not include a basket strainer.
  - Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature OH7, as described in ANSI/HI 1.1–1.2–2014.
- **End suction frame mounted (ESFM) pump** means an **end suction pump** where:
  - (1) the bare pump has its own impeller shaft and bearings and does not rely on the motor shaft to serve as the impeller shaft;
  - (2) the pump requires attachment to a rigid foundation to function as designed and cannot function as designed when supported only by the supply and discharge piping to which it is connected; and
  - (3) the pump does not include a basket strainer.
  - Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature OH0 and OH1, as described in ANSI/HI 1.1–1.2–2014.
- **In-line (IL) pump** means a single-stage, **single axis flow, rotodynamic pump** in which:
  - (1) liquid is discharged through a volute in a plane perpendicular to the impeller shaft; and
  - (2) the pump requires attachment to a rigid foundation to function as designed and cannot function as designed when supported only by the supply and discharge piping to which it is connected.
  - Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature OH3, OH4, or OH5, as described in ANSI/HI 1.1–1.2–2014.

To exclude  
circulators

To exclude dedicated-  
purpose pool pumps

# Proposed Definitions of Pump Equipment Classes (2)

- **Radially split, multi-stage, vertical, inline diffuser casing (RSV) pump** means a vertically suspended, multi-stage, **single axis flow, rotodynamic pump** in which:

(1) liquid is discharged in a plane perpendicular to the impeller shaft,

(2) each stage (or bowl) consists of an impeller and diffuser, and

(3) **no external part of such a pump is designed to be submerged in the pumped liquid.**

To exclude  
immersible

- Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature VS8, as described in ANSI/HI 2.1–2.2–2008.

- **Vertical turbine submersible (VTS) pump** means a single-stage or multistage **rotodynamic pump** that is designed to be operated with the motor and stage(s) (or bowl(s)) fully submerged in the pumped liquid, and in which:

(1) each stage of this pump consists of an impeller and diffuser, and

(2) liquid enters and exits each stage of the bare pump in a direction parallel to the impeller shaft.

- Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature VS0, as described in ANSI/HI 2.1–2.2–2008.

# Requests for Comment

**Issue 10:** DOE requests comment on its application of the proposed test procedure to the five listed pump equipment classes.

**Issue 11:** DOE requests comment on the proposed definitions for the five equipment classes.

**Issue 12:** DOE requests comment on whether the references to ANSI/HI nomenclature are (1) necessary as part of the equipment definitions in the regulatory text or (2) likely to cause confusion because of inconsistencies. DOE also seeks comment on whether discussing the ANSI/HI nomenclature in this preamble would provide sufficient reference material for manufacturers when determining the appropriate equipment class for their pump models.

# Requests for Comment

**Issue 13:** DOE requests comment on whether it needs to clarify the flow direction to distinguish RSV pumps from other similar pumps when determining test procedure and standards applicability.

**Issue 14:** DOE requests comment on whether any additional language in the RSV definition is necessary to make the exclusion of immersible pumps clearer.

**Issue 17:** DOE is interested in whether any pumps commonly referred to as ESCC, ESFM, or IL do not require attachment to a rigid foundation to function as designed.



# Circulators and Pool Pumps

- The Pumps Working Group recommended that circulator pumps and dedicated-purpose pool pumps be addressed as part of separate rulemakings.  
Pumps Working Group Recommendations # 5A, 5B
- To distinguish between circulator and dedicated-purpose pool pumps, DOE proposed design-based definitions:
  - **Circulator** means a pump that:
    - (1) is either an **end suction pump** or a single-stage, **single-axis flow, rotodynamic pump**; and
    - (2) has a pump housing that only requires the support of the supply and discharge piping to which it is connected (without attachment to a rigid foundation) to function as designed.
      - Examples include, but are not limited to, pumps complying with ANSI/HI nomenclature CP1, CP2, or CP3, as described in ANSI/HI 1.1–1.2– 2014.
  - **Dedicated-purpose pool pump** means an **end suction pump** designed specifically to circulate water in a pool and **that includes an integrated basket strainer**.
- If mutually exclusive through design, a size-based threshold is unnecessary.

Use of only pipe-mounted support provides clear and unambiguous differentiation from pumps in this rulemaking.



Use of integrated basket strainer as design feature differentiating from pumps in this rulemaking.



**Issue 16:** DOE also requests comment on the proposed definitions for circulators and dedicated-purpose pool pumps.

# Axial/Mixed Flow and Positive Displacement Pumps

- The Pumps Working Group recommended excluding axial/mixed flow and positive displacement pumps from the current rulemakings.

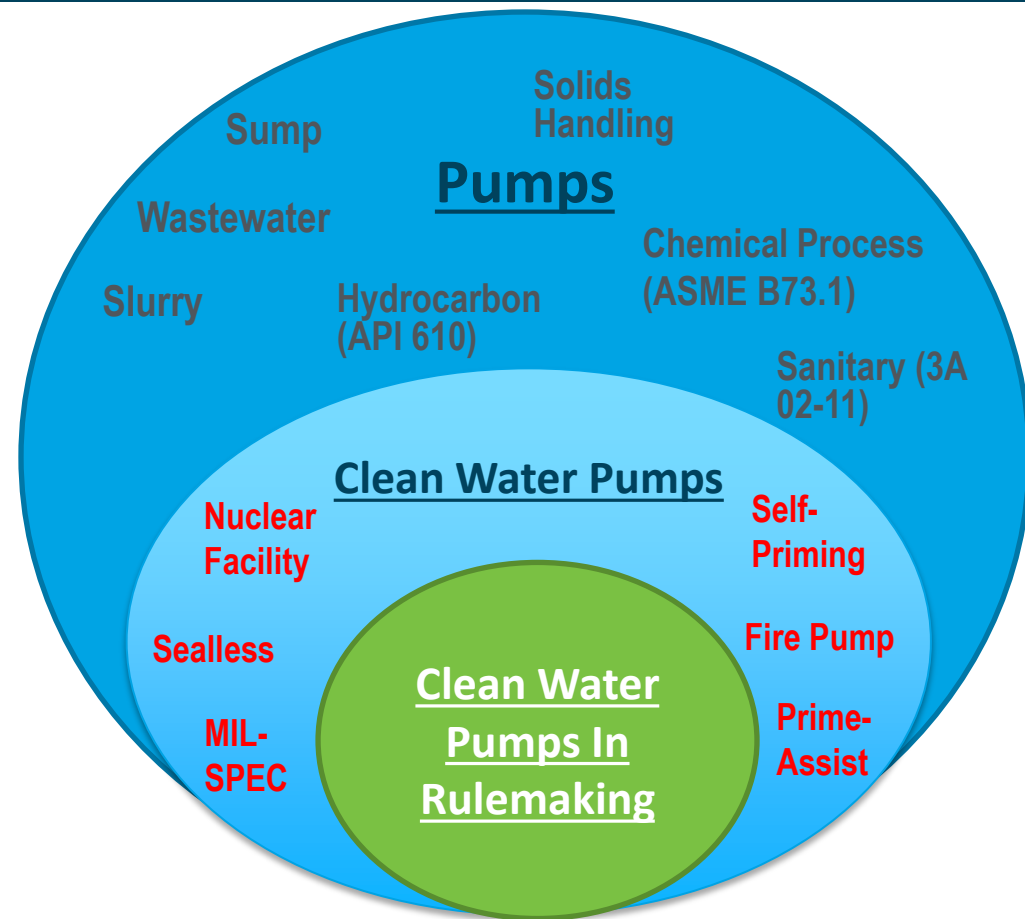
Pumps Working Group Recommendation #6

- DOE believes that the proposed definitions and scope parameters implicitly exclude these pump types.

**Issue 18:** DOE requests comment on its initial determination that axial/mixed flow and PD pumps are implicitly excluded from this rulemaking based on the proposed definitions and scope parameters. In cases where commenters suggest a more explicit exclusion be used, DOE requests comment on the appropriate changes to the proposed definitions or criteria that would be needed to appropriately differentiate axial/mixed flow and/or PD pumps from the specific rotodynamic pump equipment classes proposed for coverage in this NOPR.

# Definition of Clean Water Pump

- DOE proposed to limit the scope of the test procedure and energy conservation standards to clean water pumps, defined as follows:
  - **Clean water pump** means a pump that is designed for use in pumping water with a maximum non-absorbent free solid content of 0.25 kilograms per cubic meter, and with a maximum dissolved solid content of 50 kilograms per cubic meter, provided that the total gas content of the water does not exceed the saturation volume, and disregarding any additives necessary to prevent the water from freezing at a minimum of -10 °C.



**Issue 19:** DOE requests comment on the proposed definition for “clean water pump.”

# Requests for Comment

**Issue 21:** DOE requests comment on the proposed definition for “fire pump,” “self-priming pump,” “prime-assisted pump,” and “sealless pump.”

**Issue 22:** Regarding the proposed definition of a self-priming pump, DOE notes that such pumps typically include a liquid reservoir above or in front of the impeller to allow recirculating water within the pump during the priming cycle. DOE requests comment on any other specific design features that enable the pump to operate without manual re-priming, and whether such specificity is needed in the definition for clarity.

**Issue 23:** DOE requests comment on the proposed specifications and criteria to determine if a pump is designed to meet a specific Military Specification and if any Military Specifications other than MIL–P–17639F should be referenced.

**Issue 24:** DOE requests comment on excluding the following pumps from the test procedure: Fire pumps, self-priming pumps, prime-assist pumps, sealless pumps, pumps designed to be used in a nuclear facility, and pumps meeting the design and construction requirements set forth in Military Specification MIL–P–17639F.

# Proposed Pump Parameters

- DOE proposes to further limit the test procedure and energy conservation standards to:
  - pumps with the following performance and design characteristics:

Parameter	Criteria
Shaft Power at the Best Efficiency Point, BEP*, at Full Impeller Diameter for the Number of Stages Required for Testing to the Standard	1–200 hp
BEP Flow Rate at Full Impeller Diameter	≥25 gpm
Head at BEP at Full Impeller Diameter	≤459 feet
Design Temperature	-10 to 120 °C
Bowl Diameter for VTS Pumps (HI VSO)	≤6 inches

- And pumps designed to operate with the following styles of motors:

Style of Motor	Nominal Speed of Rotation for Rating (at 60 Hz)
2-Pole Induction Motor	3,600 rpm
4-Pole Induction Motor	1,800 rpm
Non-Induction Motor Designed to Operate Between 2,880 and 4,320 rpm	3,600 rpm
Non-Induction Motor Designed to Operate Between 1,440 and 2,160 rpm	1,800 rpm

# Proposed Definition of Bowl Diameter

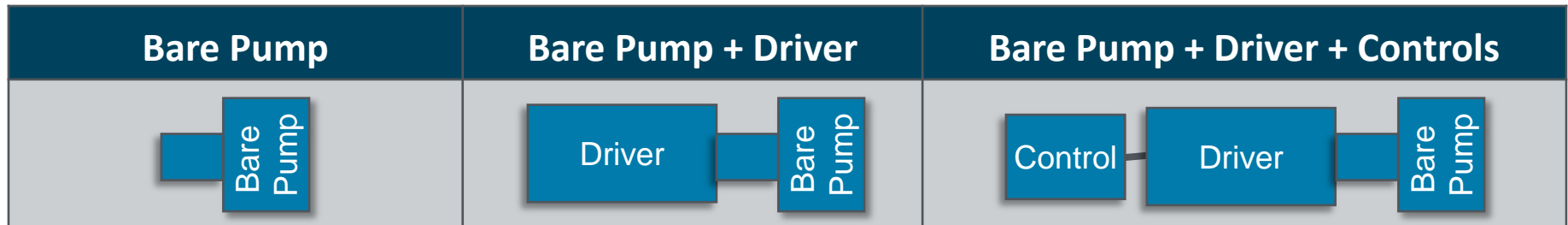
- To ensure consistent application of the design criteria related to bowl diameter, DOE proposes to define bowl diameter as follows:
  - **Bowl diameter** means the maximum dimension of an imaginary straight line passing through and in the plane of the circular shape of the intermediate bowl or chamber of the bare pump that is perpendicular to the pump shaft and that intersects the circular shape of the intermediate bowl or chamber of the bare pump at both of its ends, where the intermediate bowl or chamber is as defined in ANSI/HI 2.1–2.2–2008.

**Issue 25:** DOE requests comment on the listed design characteristics (i.e., power, flow, head, design temperature, design speed, and bowl diameter) as limitations on the scope of pumps to which the proposed test procedure would apply.

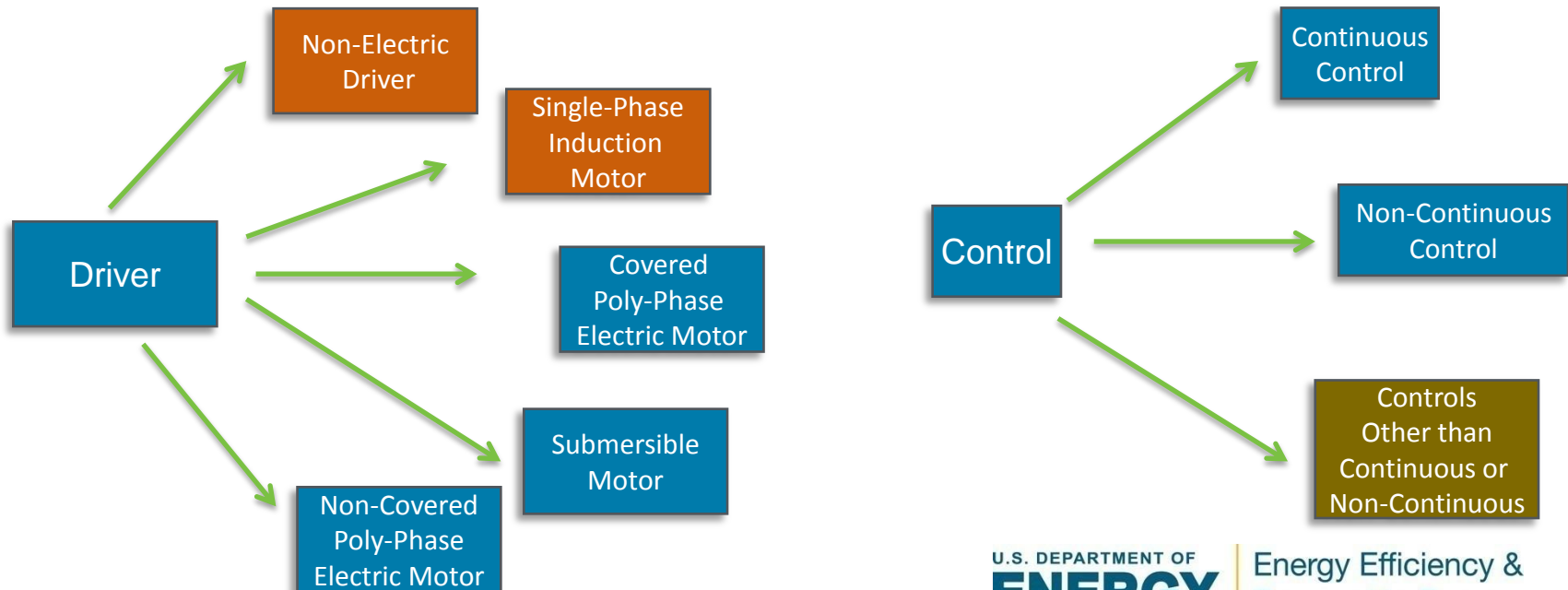
**Issue 26:** DOE requests comment on the proposed definition for “bowl diameter” as it would apply to VTS pumps.

# Pump Configurations

- The proposed test procedure and energy conservation standards would apply to pumps in three main configurations:

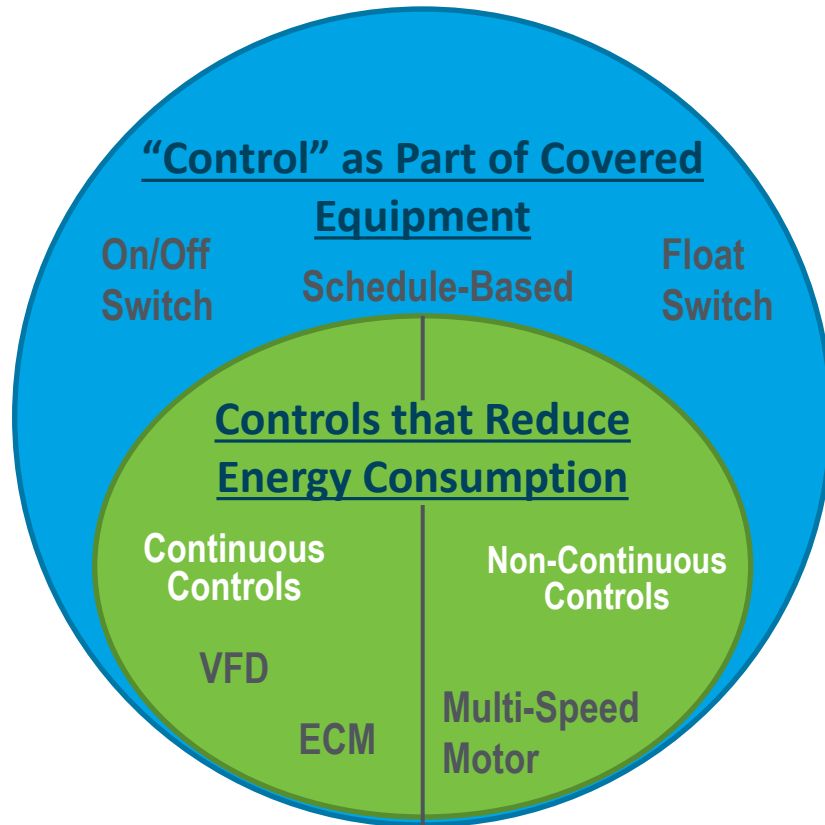


- However, the appropriate and applicable test method(s) will depend on the style of driver and control with which the pump is being rated:



# Proposed Control Category Definitions

- DOE is primarily concerned with controls that reduce pump power input at a given flow rate, specifically continuous and non-continuous controls:


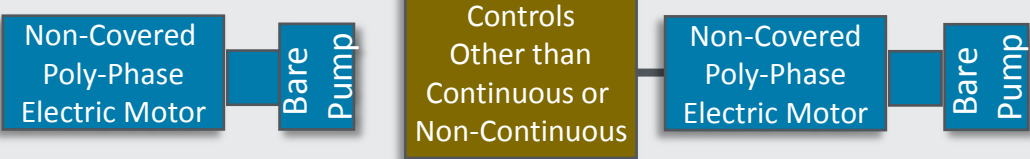
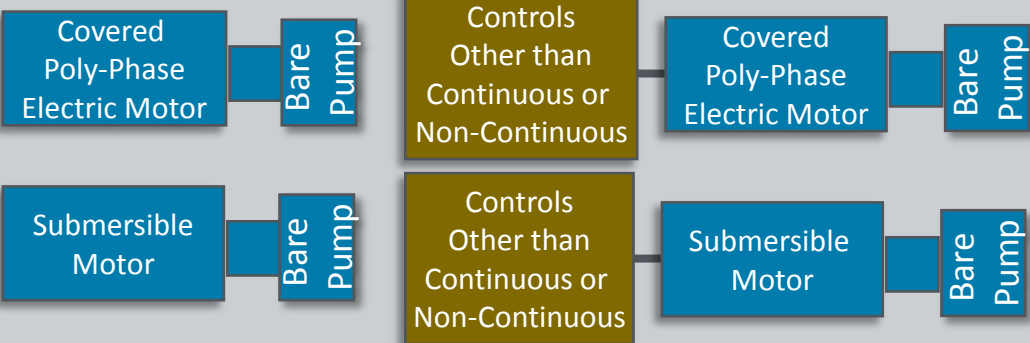
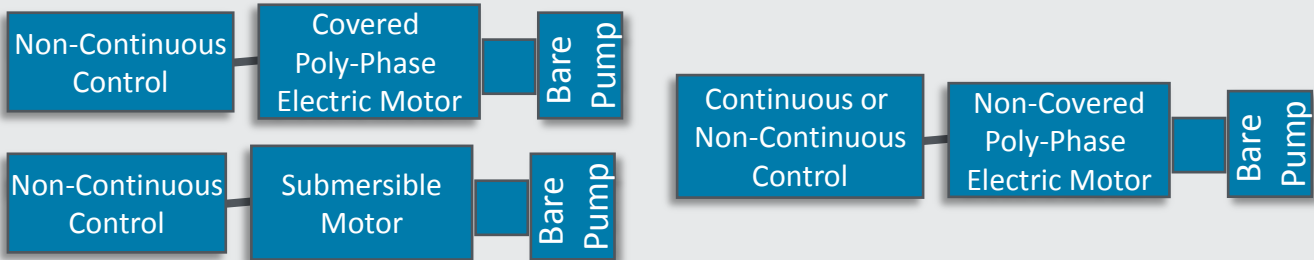



- Continuous control** means a control that adjusts the speed of the pump driver continuously over the driver operating speed range in response to incremental changes in the required pump flow, head, or power output.
- Non-continuous control** means a control that adjusts the speed of a driver to one of a discrete number of non-continuous preset operating speeds, and does not respond to incremental reductions in the required pump flow, head, or power output.

**Issue 3:** DOE requests comment on the proposed definitions for “continuous control” and “non-continuous control.”



# Rating Covered Pump Configurations

Rated As	Test Method	Applicable Pump Configurations
Bare Pump	Calculation-Based Only	 <p>Pumps Working Group Recommendation #3 (Non-Electric Drivers)</p>
Pump + Motor	Testing-Based Only	
	Testing-Based or Calculation-Based	
Pump + Motor + Controls	Testing-Based Only	
	Testing-Based or Calculation-Based	

# Requests for Comment

**Issue 27:** DOE requests comment on its proposal to test pumps sold with non-electric drivers as bare pumps.

**Issue 28:** DOE requests comment on its proposal that any pump distributed in commerce with a single-phase induction motor be tested and rated in the bare pump configuration, using the calculation method.

**Issue 29:** DOE requests comment from interested parties on any other categories of electric motors, except submersible motors, that: (1) are used with pumps considered in this rulemaking and (2) typically have efficiencies lower than the default nominal full-load efficiency for NEMA Design A, NEMA Design B, or IEC Design N motors.

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- 3 Metric
- 4 Test Procedure: Determination of Pump Performance
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- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Proposed Rating Metric

Pump Energy Index	Constant Load Pump Energy Index (PEI <sub>CL</sub> )	Variable Load Pump Energy Index (PEI <sub>VL</sub> )
Ratio	$PEI_{CL} = \left[ \frac{PER_{CL}}{PER_{STD}} \right]$	$PEI_{VL} = \left[ \frac{PER_{VL}}{PER_{STD}} \right]$
Pump Energy Rating	$PER_{CL} = \sum_i \omega_i (P^{in}_i)^*$	$PER_{VL} = \sum_i \omega_i (P^{in}_i)^*$
PER Load Profile	i = 75, 100, and 110% of BEP Flow	i = 25, 50, 75, and 100% of BEP Flow
PER <sub>STD</sub>	PER <sub>CL</sub> for Minimally Compliant Pump of the Same Equipment Class Serving the Same Hydraulic Load	
Applicable Pump Configurations	Pumps Sold without Continuous or Non-Continuous Controls	Pumps Sold with Continuous or Non-Continuous Controls
<p>*Where: <math>\omega_i</math> = weight at each load point i  <math>P^{in}_i</math> = power input to the “pump” at the driver, inclusive of the controls if present, (hp)            i = Percentage of flow at the Best Efficiency Point (BEP) of the pump</p>		

Pumps Working Group Recommendation #11

# Proposed Rating Metric Based on Pump Configuration

Metric	Rated As	Test Method	Applicable Pump Configurations
PEI <sub>CL</sub>	Bare Pump	Calculation-Based Only	
	Pump + Motor	Testing-Based Only	
		Testing-Based or Calculation-Based	
PEI <sub>VL</sub>	Pump + Motor + Controls	Testing-Based Only	
		Testing-Based or Calculation-Based	

# Requests for Comment

**Issue 30:** DOE requests comment on the proposed load points and weighting for  $PEI_{CL}$  for bare pumps and pumps sold with motors and  $PEI_{VL}$  for pumps inclusive of motors and continuous or non-continuous controls.

**Issue 31:** DOE requests comments on the proposed  $PEI_{CL}$  and  $PEI_{VL}$  metric architecture.

# Determining PEI

- The PEI represents the performance of the pump, motor, and controls, if present.

Metric	Rated As	Test Method	Bare Pump Performance	Motor Performance	Controls Performance
PEI <sub>CL</sub>	Bare Pump	Calculation-Based Only	Tested	Minimally Compliant Motor Efficiency with Assumed Part-Load Losses	N/A
	Pump + Motor	Testing-Based Only	Tested		N/A
		Testing-Based or Calculation-Based	Tested	Nominal Motor Efficiency with Assumed Part-Load Losses	N/A
PEI <sub>VL</sub>	Pump + Motor + Controls	Testing-Based Only	Tested		
		Testing-Based or Calculation-Based	Tested	Nominal Motor Efficiency	Assumed System Curve and Assumed Part-Load Losses of Motor + Controls

# Determining $PEI_{CL}$ for an Uncontrolled Pump

$$PEI_{CL} = \left[ \frac{PER_{CL}}{PER_{STD}} \right]$$

$$= \left[ \frac{\omega_{75\%}(P^{in}_{75\%}) + \omega_{100\%}(P^{in}_{100\%}) + \omega_{110\%}(P^{in}_{110\%})}{PER_{STD}} \right] = \left[ \frac{\frac{1}{3}*(P_{75\%} + L_{75\%}) + \frac{1}{3}*(P_{100\%} + L_{100\%}) + \frac{1}{3}*(P_{110\%} + L_{110\%})}{PER_{STD}} \right]$$

Testing-Based Approach	Calculation-Based Approach
<ul style="list-style-type: none"> <li>• Tested driver input power (<math>P^{in}_{100\%}</math>) is measured directly                             <ul style="list-style-type: none"> <li>– <math>P_i</math> values are the tested input power to the driver (motor) at each load point <math>i</math>.                                     <ul style="list-style-type: none"> <li>• <math>i = 75\%, 100\%</math>, and <math>110\%</math> of flow rate at BEP of the bare pump</li> <li>• Equal weighting</li> </ul> </li> <li>– Reflects the performance of both the bare pump and the motor.</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>• <b>Bare Pump Performance</b> <ul style="list-style-type: none"> <li>– <math>P_i</math> values are the tested shaft input power to the pump (speed x torque) at each load point <math>i</math>.                                     <ul style="list-style-type: none"> <li>• <math>i = 75\%, 100\%</math>, and <math>110\%</math> of flow rate at BEP of the bare pump</li> <li>• Equal weighting</li> </ul> </li> </ul> </li> <li>• <b>Motor Performance (Losses)</b> <ul style="list-style-type: none"> <li>– <math>L_i</math> is either:                                     <ul style="list-style-type: none"> <li>• (A) the part-load losses of a motor that is paired with the pump for pumps sold with motors or</li> <li>• (B) the part-load losses of an open or enclosed motor that is minimally compliant with DOE's motor regulations (10 CFR 431.25) for NEMA Design A, Design B, IEC Design N Electric Motors except for submersible motors, sized based on shaft input power of the pump evaluated at 120% of BEP flow</li> </ul> </li> </ul> </li> </ul>
<ul style="list-style-type: none"> <li>• <b>No Controls</b></li> </ul>	<ul style="list-style-type: none"> <li>• <b>No Controls</b></li> </ul>



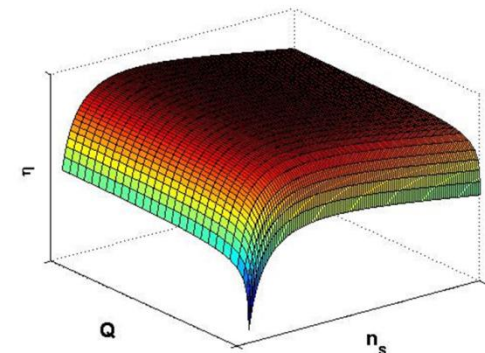
# PER<sub>STD</sub>: Minimally Compliant Pump

- PER<sub>STD</sub> is equivalent to PER<sub>CL</sub> for a minimally compliant pump
  - Based on the tested characteristics and hydraulic load of the **pump being rated**.
  - Assumes a pump curve shape for the minimally compliant pump and always assumes no controls.
  - **Motor losses** are that of a minimally compliant open or enclosed motor for the appropriate pump equipment class, horsepower configuration, and speed.
  - The **minimally compliant pump efficiency** is calculated for **each pump equipment class** based on a function of flow and speed of the **pump being rated**.

$$PER_{STD} = \omega_{75\%} \left( \frac{P_{Hydro,75\%}}{0.95 * \eta_{pump,STD}} + L_{75\%} \right) + \omega_{100\%} \left( \frac{P_{Hydro,100\%P}}{\eta_{pump,STD}} + L_{100\%} \right) + \omega_{110\%} \left( \frac{P_{1.10\%}}{0.985 * \eta_{pump,STD}} + L_{110\%} \right)$$

$$\eta_{pump,STD} = -0.85 * \ln(Q_{100\%})^2 - 0.38 * \ln(Ns) * \ln(Q_{100\%}) - 11.48 * \ln(Ns)^2 + 17.80 * \ln(Q_{100\%}) + 179.80 * \ln(Ns) - (C + 555.6)$$

Where: Ns = the specific speed at 60 Hz,  
 Q = the flow rate of the pump at BEP in GPM,  
 C = the C-value of the surface, which is set based on the speed of rotation of the pump, and the pump equipment class



# Determining $PEI_{VL}$ for a Controlled Pump

$$PEI_{VL} = \left[ \frac{PER_{VL}}{PER_{STD}} \right]$$

$$= \left[ \frac{\omega_{25\%}(P^{in}_{25\%}) + \omega_{50\%}(P^{in}_{50\%}) + \omega_{75\%}(P^{in}_{75\%}) + \omega_{100\%}(P^{in}_{100\%})}{PER_{STD}} \right]$$

$$= \left[ \frac{\frac{1}{4}(P_{25\%} + L_{25\%}) + \frac{1}{4}(P^{in}_{50\%} + L_{50\%}) + \frac{1}{4}(P^{in}_{75\%} + L_{75\%}) + \frac{1}{4}(P^{in}_{100\%} + L_{100\%})}{PER_{STD}} \right]$$

Testing-Based Approach	Calculation-Based Approach
<ul style="list-style-type: none"> <li>• Tested driver input power (<math>P^{in}_{100\%}</math>) is measured directly               <ul style="list-style-type: none"> <li>– <math>P_i</math> values are the tested input power to the driver (control) at each load point <math>i</math>.                   <ul style="list-style-type: none"> <li>• <math>i = 25\%, 50\%, 75\%</math>, and <math>100\%</math> of flow rate at BEP of the bare pump</li> <li>• Equal weighting</li> </ul> </li> <li>– Reflects the performance of the bare pump, motor, and control.</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>• <b>Pump Performance</b> <ul style="list-style-type: none"> <li>– <math>P_{in}</math> values are the input electrical power to the drive a load point <math>i</math>.                   <ul style="list-style-type: none"> <li>• <math>i = 25\%, 50\%, 75\%</math>, and <math>100\%</math> of flow rate at BEP of the pump</li> <li>• Equal weighting</li> </ul> </li> </ul> </li> </ul>
<ul style="list-style-type: none"> <li>• <b>Controls Performance</b> <ul style="list-style-type: none"> <li>– Benefit is captured in the calculation of bare shaft input power.</li> <li>– Accounts for drive efficiency in tested driver input power.</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>• <b>Motor Performance (Losses)</b> <ul style="list-style-type: none"> <li>– <math>L_i</math> is the part-load losses of motor and control that are paired with the pump</li> </ul> </li> <li>• <b>Controls Performance</b> <ul style="list-style-type: none"> <li>– Benefit is captured in the calculation of bare shaft input power.</li> <li>– Accounts for drive efficiency in calculated losses</li> </ul> </li> </ul>

# Request for Comment

**Issue 32:** DOE requests comment on its proposal to base the default motor horsepower for the minimally compliant pump on that of the pump being evaluated. That is, the motor horsepower for the minimally compliant pump would be based on the calculated pump shaft input power of the pump when evaluated at 120 percent of BEP flow for bare pumps and the horsepower of the motor with which that pump is sold for pumps sold with motors (with or without continuous or non-continuous controls).

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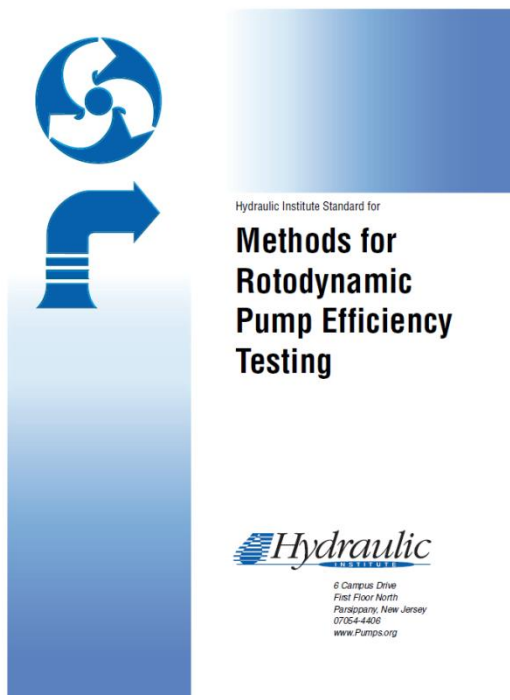
# Determination of Pump Performance

- To determine  $PEI_{CL}$  or  $PEI_{VL}$ , as applicable, the input power to the pump at the specified load points is required.
- The proposed test procedure requires physically measuring either:
  - the bare pump (for calculation-based methods), or
  - the entire pump, inclusive of any motor, continuous control, or non-continuous control (for testing-based methods).
- DOE's test procedure, as proposed, requires instructions for how to physically measure the performance of bare pumps, pumps with motors, and pumps with motors and continuous or non-continuous controls in a standardized and consistent manner.

# Referenced Industry Standards

- Consistent with Working Group Recommendations, DOE proposes to incorporate by reference the Hydraulic Institute (HI) Standard 40.6–2014, “Methods for Rotodynamic Pump Efficiency Testing,” as part of DOE’s test procedure for measuring the energy consumption of pumps, **with a few minor modifications**.

HI 40.6-2014



Proposed Minor Modifications Include:	
Exclude sections not relevant to DOE’s regulatory framework	Section 40.6.5.3 and appendix B (reporting) & section A.7 (high temperature testing)
Specify data collection interval	Collect data every 5 seconds
Specify allowable integration of data for stabilization	Dampening devices cannot integrate over time periods $\geq 5$ seconds
Improve test repeatability	<b>Pumps speed, power supply characteristics, number of stages for multi-stage pumps, determination of pump shaft input power, electrical measurement equipment,</b> pumps with BEP at run-out, calculations and rounding

Pumps Working Group Recommendation # 10 (with slight modifications)

**Issue 33:** DOE requests comment on using HI 40.6–2014 as the basis of the DOE test procedure for pumps.

# Pump Speed

- HI 40.6–2014 does not clearly specify nominal rating speeds for tested pump models.
- DOE proposes that all test data be adjusted (in accordance with section 40.6.6.1.1) to the following nominal speed prior to use in subsequent calculations:

Pump Configuration	Pump Design Speed of Rotation	Style of Motor	Nominal Speed of Rotation for Rating
Bare Pump	2,880 and 4,320 rpm	N/A	3,600 rpm
	1,440 and 2,160 rpm		1,800 rpm
Pump + Motor OR Pump + Motor + Control	N/A	2-Pole Induction Motor	3,600 rpm
	N/A	4-Pole Induction Motor	1,800 rpm
	N/A	Non-Induction Motor Designed to Operate Between 2,880 and 4,320 rpm	3,600 rpm
	N/A	Non-Induction Motor Designed to Operate Between 1,440 and 2,160 rpm	1,800 rpm

- Consistent with HI 40.6–2014, DOE proposes that the tested speed must be maintained within 20 percent of the nominal speed, and the speed of rotation recorded at each test point may not vary more than  $\pm 1$  percent to ensure accurate and reliable results.

# Requests for Comment

**Issue 37:** DOE requests comment on its proposal to require data collected at the pump speed measured during testing to be normalized to the nominal speeds of 1,800 and 3,600 rpm.

**Issue 38:** DOE requests comment on its proposal to adopt the requirements in HI 40.6–2014 regarding the deviation of tested speed from nominal speed and the variation of speed during the test. Specifically, DOE is interested if maintaining the tested speed within  $\pm 1$  percent of the nominal speed is feasible and whether this approach would produce more accurate and repeatable test results.



# Power Supply Characteristics

- To determine the appropriate power supply characteristics for testing pumps with motors and pumps with both motors and continuous or non-continuous controls, DOE examined applicable test methods for electric motors and VSD systems.

Test Procedure	Applicable Equipment	Voltage Requirement	Frequency Requirement	Total Harmonic Distortion	Impedance
IEEE Standard 112–2004	Electric Motors	Maintained Within $\pm 0.5\%$ and “Voltage Unbalance” $\leq 0.5\%$	Maintained Within $\pm 0.5\%$	<5%	N/A
AHRI 1210–2011	Variable Speed Drives			N/A	$\leq 1\%$
CSA C838–2013	Variable Speed Drives			<5%	>1% and $\leq 3\%$

- DOE proposes to establish **these power supply requirements** in the DOE pump test procedure for measurement of electric input power to the motor or controls.

**Issue 39:** DOE requests comment on the proposed voltage, frequency, voltage unbalance, total harmonic distortion, and impedance requirements that are required when performing a wire-to-water pump test or when testing a bare pump with a calibrated motor. Specifically, DOE requests comments on whether these tolerances can be achieved in typical pump test labs, or whether specialized power supplies or power conditioning equipment would be required.

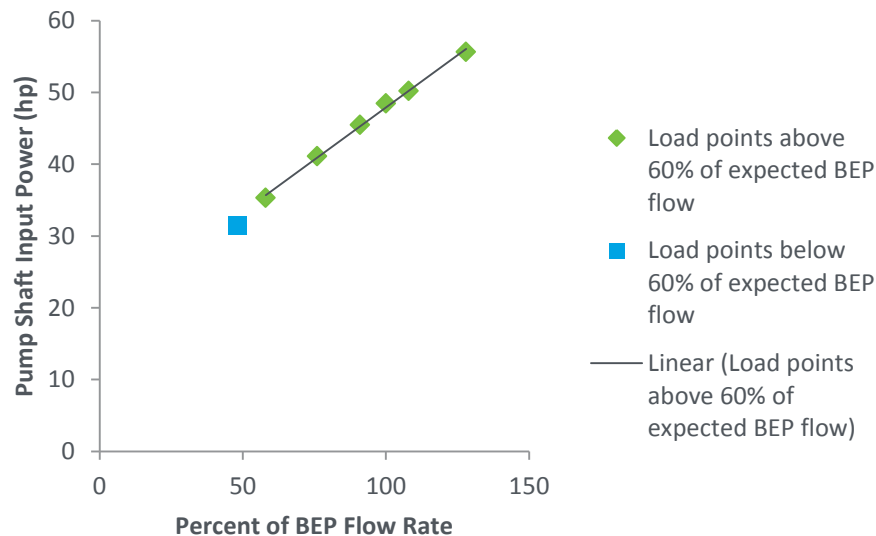
# Measurement Equipment for Testing of Controlled Pumps

- When measuring input power to the pump for pumps sold with a motor and continuous or non-continuous controls, the equipment specified in section C.4.3.1, “electric power input to the motor,” of HI 40.6–2014 may not be sufficient.
- CSA C838–2013 and AHRI 1210–2011 require that electrical measurements for determining variable speed drive efficiency be taken using equipment:
  - capable of measuring current, voltage, and real power up to at least the 40th harmonic of fundamental supply source frequency and
  - having an accuracy level of  $\pm 0.2$  percent of full scale when measured at the fundamental supply source frequency.
- DOE proposes that the electrical measurement equipment specified in AHRI 1210–2011 and CSA C838–2013 be required for the purposes of measuring input power to a pump sold with a motor and continuous or non-continuous controls.

**Issue 43:** DOE requests comment on the type and accuracy of required measurement equipment, especially the equipment required for electrical power measurements for pumps sold with motors having continuous or non-continuous controls.

# Pump Shaft Input Power at Load Points

- The test protocol in HI 40.6–2014 requires that test data be collected at 40, 60, 75, 90, 100, 110, and 120 percent of the expected BEP flow.\*
  - HI 40.6–2014 does not specify how to determine relevant parameters at the specific load points (i.e., 75, 100, or 110 percent of the *actual* BEP flow for  $PER_{CL}$  and  $PER_{STD}$ ).
- DOE proposes that the pump shaft input power at the specific load points of 75, 100, and 110 percent of *expected* BEP flow be determined by regressing the pump shaft input power with respect to flow for the measured data at the load points between 60 and 110 percent of expected BEP flow.



**Issue 41:** DOE requests comment on its proposal to use a linear regression of the pump shaft input power with respect to flow rate at all the tested flow points greater than or equal to 60 percent of expected BEP flow to determine the pump shaft input power at the specific load points of 75, 100, and 110 percent of BEP flow. DOE is especially interested in any pump models for which such an approach would yield inaccurate measurements.

\* For pumps with BEP at run-out data shall be collected at 40, 50, 60, 70, 80, 90, and 100% of expected BEP flow

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# Determining of Motor Efficiency

- Default motor efficiency, or motor losses, are required for determining the  $PER_{CL}$  of a bare pump or the  $PER_{STD}$  for any pump configuration.

	Nominal Full-Load Motor Efficiency		Default Full-Load Motor Efficiency	
Metric Applicability	$PER_{CL}$ or $PER_{VL}$ for pumps + motors and pumps + motors + controls		$PER_{CL}$ for Bare Pumps	$PER_{STD}$ for All Pumps
Default Nominal Motor Full-Load Efficiency for Pumps Rated with...	Covered Poly-Phase Electric Motor	Measured Nominal Full-Load Efficiency Determined in Accordance with the DOE Electric Motor Test Procedure Specified at 10 CFR 431.16 and Appendix B to Subpart B of Part 431	Nominal Full-Load Motor Efficiency (Standard) for General Purpose, Polyphase, NEMA Design A, NEMA Design B, and IEC Design N Motors Defined at 10 CFR 431.25	
	Non-Covered Poly-Phase Electric Motor	Not Applicable (Only Testing-Based Approach can be Used)	Nominal Full-Load Motor Efficiency (Standard) for General Purpose, Polyphase, NEMA Design A, NEMA Design B, and IEC Design N Motors Defined at 10 CFR 431.25	
	Submersible Motor	Default Submersible Motor Full-Load Efficiency	Default Submersible Motor Full-Load Efficiency	Default Submersible Motor Full-Load Efficiency
Default Motor Speed	Equivalent to nominal speed of the rated pump			
Default Motor Horsepower	That of the motor with which the pump is being sold		Either equivalent to, or the next highest horsepower-rated level greater than, the measured pump shaft input power at 120 percent of BEP flow	That of the motor with which the pump is being sold

# Default Motor Efficiencies at 10 CFR 431.25

Motor horsepower	Default Nominal Full-Load Motor Efficiency (%)		Nominal Full-Load Efficiencies (%) of NEMA Design A, NEMA Design B and IEC Design N Motors (Excluding Fire Pump Electric Motors) at 60 Hz			
	Minimum Efficiency (%)		Enclosed Motors		Open Motors	
	Number of Poles		Number of Poles		Number of Poles	
	4	2	4	2	4	2
1	77.0	77.0	85.5	77.0	85.5	77.0
1.5	84.0	84.0	86.5	84.0	86.5	84.0
2	85.5	85.5	86.5	85.5	86.5	85.5
3	85.5	86.5	89.5	86.5	89.5	85.5
5	86.5	88.5	89.5	88.5	89.5	86.5
7.5	88.5	89.5	91.7	89.5	91.0	88.5
10	89.5	90.2	91.7	90.2	91.7	89.5
15	90.2	91.0	92.4	91.0	93.0	90.2
20	91.0	91.0	93.0	91.0	93.0	91.0
25	91.7	91.7	93.6	91.7	93.6	91.7
30	91.7	91.7	93.6	91.7	94.1	91.7
40	92.4	92.4	94.1	92.4	94.1	92.4
50	93.0	93.0	94.5	93.0	94.5	93.0
60	93.6	93.6	95.0	93.6	95.0	93.6
75	93.6	93.6	95.4	93.6	95.0	93.6
100	93.6	94.1	95.4	94.1	95.4	93.6
125	94.1	95.0	95.4	95.0	95.4	94.1
150	94.1	95.0	95.8	95.0	95.8	94.1
200	95.0	95.4	96.2	95.4	95.8	95.0
250	95.0	95.8	96.2	95.8	95.8	95.0

10 CFR 431.25(h)

# Requests for Comment

**Issue 45:** DOE requests comment on its proposal to determine the default motor horsepower for rating bare pumps based on the pump shaft input power at 120 percent of BEP flow. DOE is especially interested in any pumps for which the 120 percent of BEP flow load point would not be an appropriate basis to determine the default motor horsepower (e.g., pumps for which the 120 percent of BEP flow load point is a significantly lower horsepower than the BEP flow load point).

**Issue 46:** DOE requests comment on its proposal that would specify the default, minimally compliant nominal full-load motor efficiency based on the applicable minimally allowed nominal full-load motor efficiency specified in DOE's energy conservation standards for NEMA Design A, NEMA Design B, and IEC Design N motors at 10 CFR 431.25 for all pumps except pumps sold with submersible motors.



# Default Submersible Motor Full-Load Efficiency

- Submersible motors are not currently subject to the DOE energy conservation standards for electric motors specified at 10 CFR 431.25.
- DOE proposes to establish a default table of motor efficiencies for submersible motors to pair with VTS pumps when using the calculation method or calculating the  $PER_{STD}$ .
  - DOE determined representative minimum submersible motor efficiencies from literature review and data mining.
  - DOE specified the submersible motor efficiency based on the number of “bands” below comparable NEMA Design A, NEMA Design B, or IEC Design N motors of the same horsepower.

Motor Horse power (hp)	Minimum Observed Full-Load Efficiency (2-poles) (%)	Observed Number of “Bands” Below the Full-Load Efficiency in Table 5 of 10 CFR 431.25(h)	Default Number of “Bands” Below the Full-Load Efficiency in Table 5 of 10 CFR 431.25(h)	Default Submersible Motor Full-Load Nominal Efficiency	
				2-pole	4-pole
1	67	6	11	55	68
1.5	67	11		66	70
2	73	9		68	70
3	75	9		70	75.5
5	76	10		74	75.5
7.5	77	10	15	68	74
10	75	13		70	74
15	72.2	15		72	75.5
20	76.4	13		72	77
25	79	12		74	78.5
30	79.9	12	12	78.5	82.5
40	83	10		80	84
50	83	11		81.5	85.5
60	84	11		82.5	86.5
75	83.8	12		82.5	87.5
100	87	10	14	81.5	85.5
125	86	13		84	85.5
150	86	13		84	86.5
175	88	12		85.5	87.5
200	87	14		86.5	87.5
250	87	14		55	68

# Requests for Comment

**Issue 47:** DOE requests comment on the proposed default minimum full-load motor efficiency values for submersible motors.

**Issue 48:** DOE requests comment on defining the proposed default minimum motor full-load efficiency values for submersible motors relative to the most current minimum efficiency standards levels for regulated electric motors, through the use of “bands.”

**Issue 49:** DOE requests comment on the proposal to allow the use of the default minimum submersible motor full-load efficiency values to rate: (1) VTS bare pumps, (2) pumps sold with submersible motors, and (3) pumps sold with submersible motors and continuous or non-continuous controls as an option instead of wire-to-water testing.

# Part-Load Motor Losses

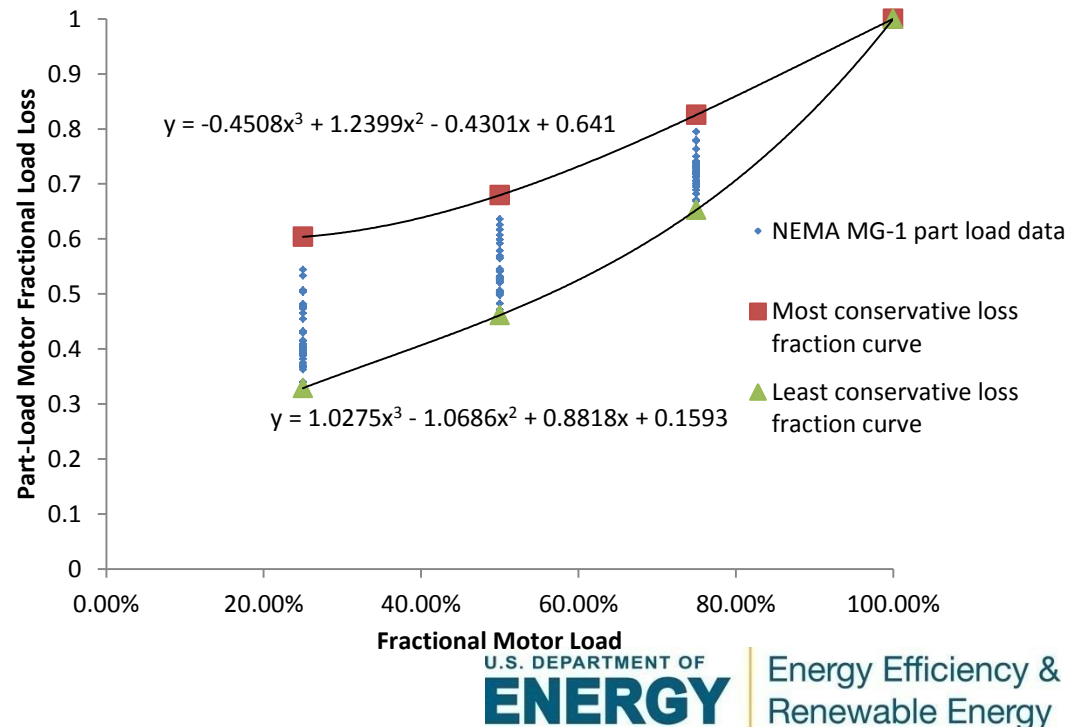
- When calculating  $PER_{STD}$  or  $PER_{CL}$  for all pumps the part-load motor losses at each load point must be determined:  $P^{in}_i = P_i + L_i$
- DOE proposes to determine part-load motor losses based on a “part-load loss factor” and the full-load motor losses:

Step	Equation	Where
1. Calculate full-load losses for the motor.	$L_{full,default} = \frac{MotorHP}{[\eta_{motor,full}/100]} - MotorHP$	$L_{full,default}$ = default (or nominal) motor losses at full-load (hp), $\eta_{motor,full}$ = the full-load motor efficiency
2. Determine the part-load loss factor ( $y_i$ ) for each rating point, where part-load loss factor at a given point represents the part-load losses at the given load divided by full-load losses.	$y_i = \left( -0.4508 \times \left( \frac{P_i}{MotorHP} \right)^3 + 1.2399 \times \left( \frac{P_i}{MotorHP} \right)^2 - 0.4301 \times \left( \frac{P_i}{MotorHP} \right) + 0.6410 \right)$	$y_i$ = the part-load loss factor at load point $i$ , $P_i$ = the shaft input power to the bare pump (hp), $MotorHP$ = the motor horsepower (hp) $i$ = percentage of flow at the BEP of the pump.
3. Multiply the full-load losses by each part-load loss factor to obtain part-load losses at each rating point.	$L_i = L_{full,default} \times y_i$	$L_i$ = default motor losses at rating point $i$ (hp)

# Determination of Part-Load Loss Curve

- DOE evaluated motor efficiency data at 25, 50, 75, and 100 percent of full-load of the motor from multiple sources, including NEMA, the DOE MotorMaster database, and the DOE Motor Challenge.
  - DOE considered providing multiple part-load loss curves based on motor size, motor speed, and/or motor type, but ultimately determined that the rating metric is not sensitive to changes in the part-load loss curve based on these factors.
  - Therefore, DOE proposes to adopt a single curve represented by a cubic polynomial for determining the part-load losses of motors when using the calculation method.

**Issue 50:** DOE requests comment on the development and use of the motor part-load loss factor curves to describe part-load performance of covered motors and submersible motors including the default motor specified for bare pumps and calculation of  $PER_{STD}$ .



# Public Meeting Slides Topics – Morning (TP)

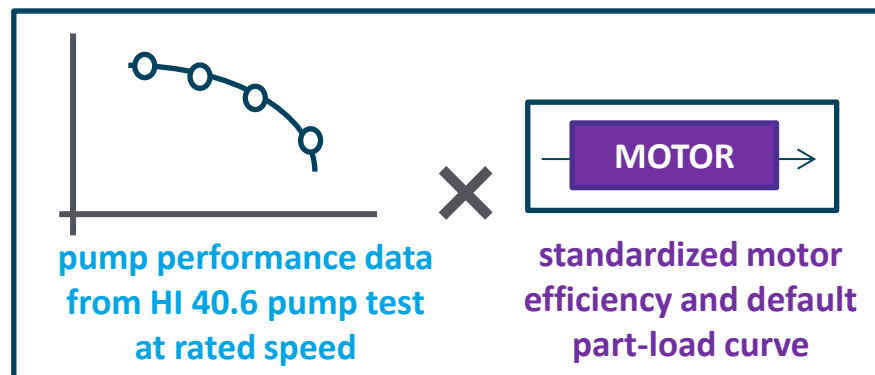
- 1 Introductions & Stakeholder Opening Statements
- 2 Regulatory History & Scope
- 3 Metric
- 4 Test Procedure: Determination of Pump Performance
- 5 Break
- 6 Test Procedure: Determination of Driver Efficiency
- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Testing Methods: Calculation- and Testing-Based

- DOE considered both testing-based and calculation-based methods for determining the metric for a given pump configuration.

Test Method	Pros	Cons
Calculation Based Approach	Repeatable; Less Burdensome	Assumptions Regarding Change in Motor/Controls Efficiency with Changing Load Required; Decreased Accuracy; Not applicable to ALL pumps
Testing Based Approach	Accurate; Differentiates Performance of Different Motor/Controls Equipment at Full and Part-Load	Burdensome

# Calculation-Based: A.1 – Bare Pump



- The bare pump  $PER_{CL}$  would be measured based on the pump shaft input power at 75, 100, and 110 percent of BEP flow.

$$PER_{CL} = \omega_{75\%}(P_{75\%}^{in}) + \omega_{100\%}(P_{100\%}^{in}) + \omega_{110\%}(P_{110\%}^{in})$$

$$= \omega_{75\%}(P_{75\%} + L_{75\%}) + \omega_{100\%}(P_{100\%} + L_{100\%}) + \omega_{110\%}(P_{110\%} + L_{110\%})$$

Where:

$\omega_i$  = weighting at each rating point (equal weighting or  $1/3$  in this case),

$P_i^{in}$  = calculated input power to the motor at rating point  $i$  (hp),

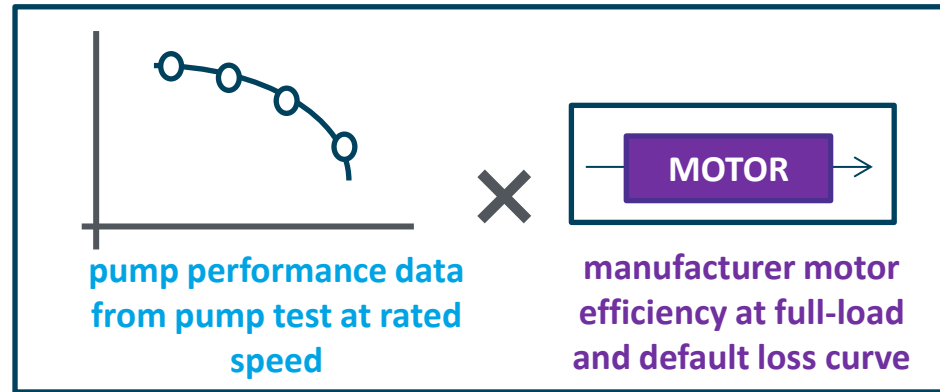
$P_i$  = the tested shaft input power to the bare pump (hp),

$L_i$  = default motor losses at each load point  $i$  (hp), and

$i$  = 75, 100, and 110 percent of BEP flow as determined in accordance with the DOE test procedure.

$$PEI_{CL} = \left[ \frac{PER_{CL}}{PER_{STD}} \right]$$

# Calculation-Based: B.1 – Pump Sold With a Motor



- Procedure is the same as for pumps sold as bare pumps except that motor efficiency, or losses, would be that of the motor with which the pump is sold when determining  $PER_{CL}$ , as opposed to the default motor efficiency.

$$PER_{CL} = \omega_{75\%}(P_{75\%}^{in}) + \omega_{100\%}(P_{100\%}^{in}) + \omega_{110\%}(P_{110\%}^{in})$$

$$= \omega_{75\%}(P_{75\%} + L_{75\%}) + \omega_{100\%}(P_{100\%} + L_{100\%}) + \omega_{110\%}(P_{110\%} + L_{110\%})$$

Where:

$\omega_i$  = weighting at each rating point (equal weighting or  $1/3$  in this case),

$P_i^{in}$  = calculated input power to the motor at rating point  $i$  (hp),

$P_i$  = the tested shaft input power to the bare pump (hp),

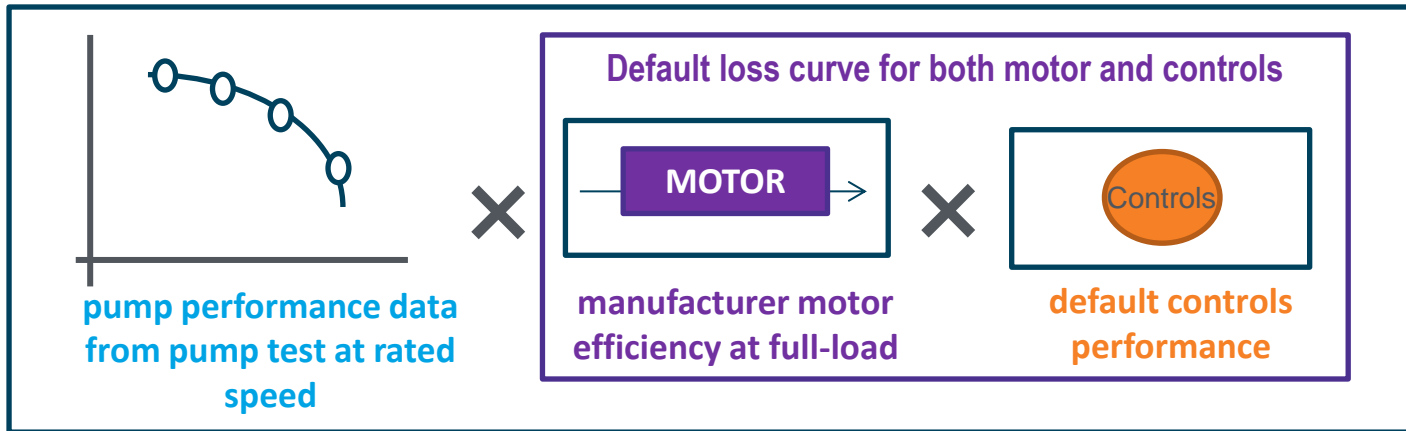
$L_i$  = default motor losses at each load point  $i$  (hp), and

$i = 75, 100,$  and  $110$  percent of BEP flow as determined in accordance with the DOE test procedure.

determined based on nominal full-load efficiency of motor with which pump is being rated



# Calculation-Based: C.1 – Pump, Motor & Continuous Control



- $PEI_{VL}$  accounts for the power reduction resulting from continuous controls.

$$\begin{aligned}
 PER_{VL} &= \omega_{25\%}(P_{25\%}^{in}) + \omega_{50\%}(P_{50\%}^{in}) + \omega_{75\%}(P_{75\%}^{in}) + \omega_{100\%}(P_{100\%}^{in}) \\
 &= \omega_{25\%}(P_{25\%} + L_{25\%}) + \omega_{50\%}(P_{50\%} + L_{50\%}) + \omega_{75\%}(P_{75\%} + L_{75\%}) + \omega_{100\%}(P_{100\%} + L_{100\%})
 \end{aligned}$$

Where:

$\omega_i$  = weighting at each rating point (equal weighting or ¼ in this case),

$P_i^{in}$  = measured or calculated input power to the pump at the input to the continuous or non-continuous controls at rating point  $i$ , and

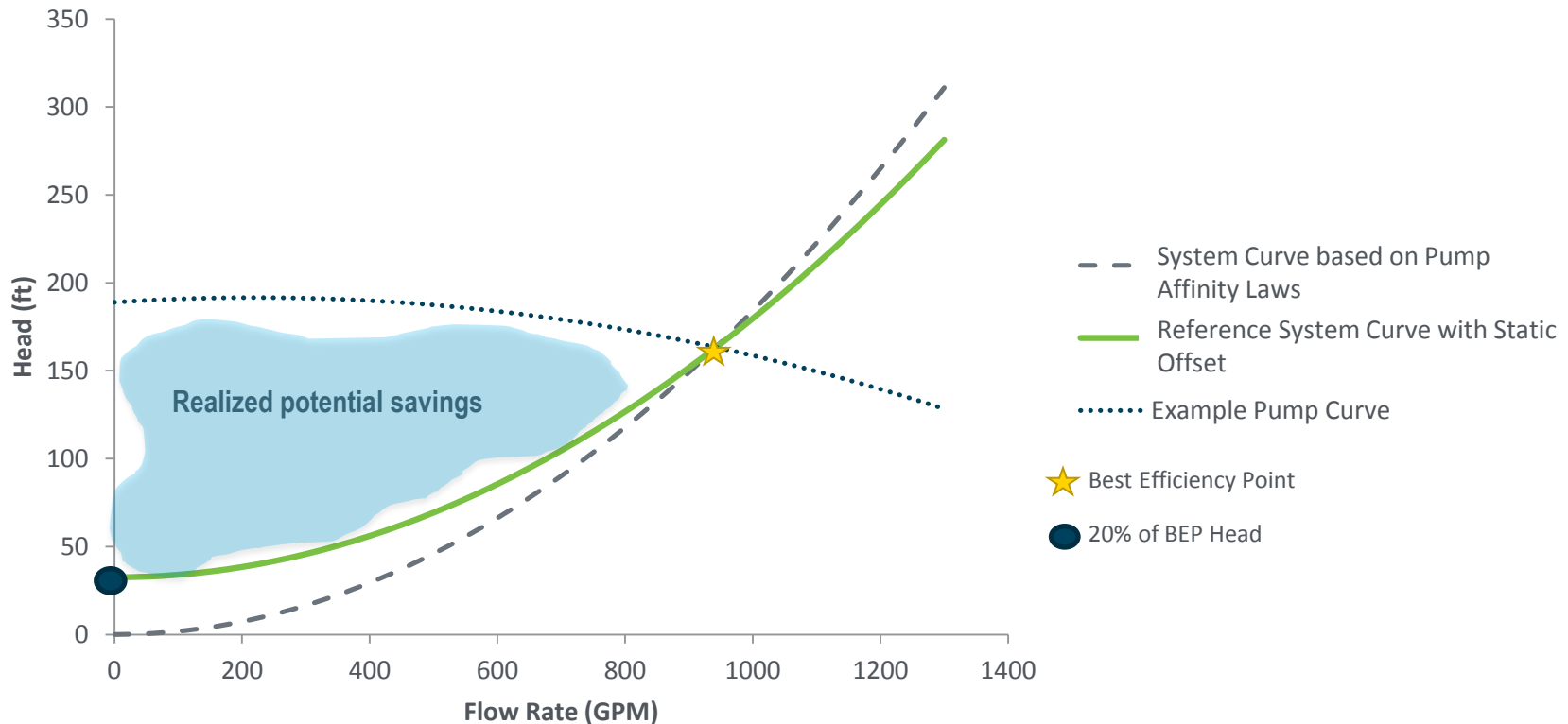
$P_i$  = the tested shaft input power to the bare pump (hp),

$L_i$  = default motor and control losses at each load point  $i$  (hp), and

$i$  = 25, 50, 75, and 100 percent of BEP flow, as determined in accordance with the proposed DOE test procedure.

# Reference System Curve

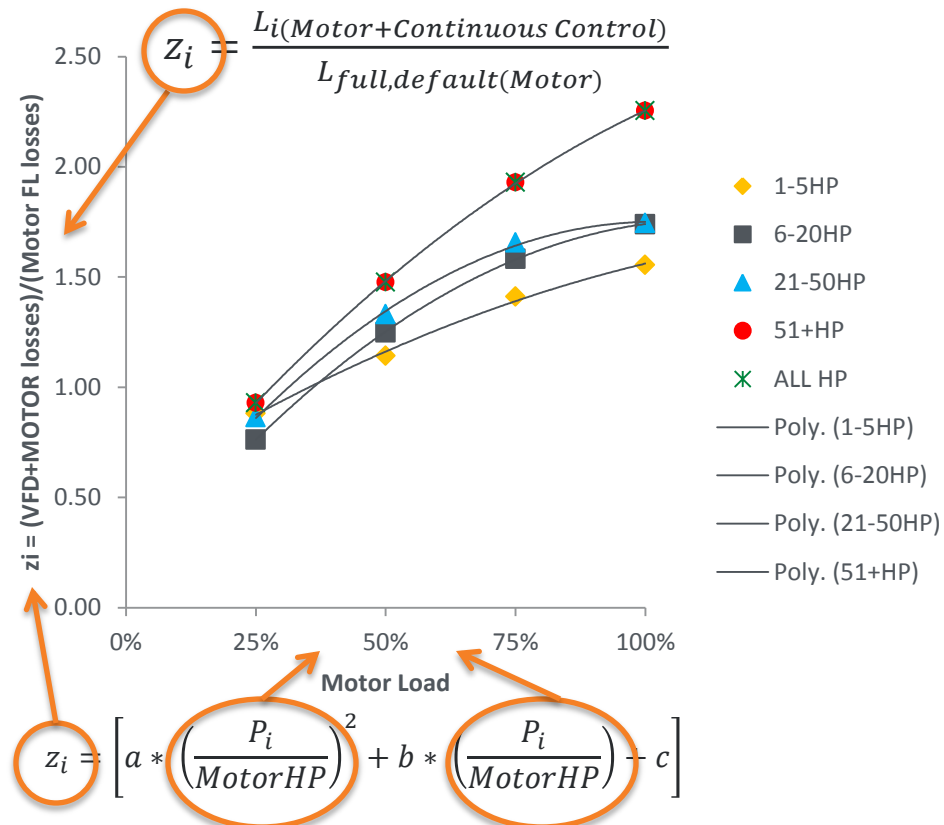
- DOE proposes a reference system curve based on the pump affinity laws, but with a static offset.
  - Static head offset is 20% of BEP head.
  - Given  $Q_{BEP}$  and  $H_{BEP}$ , the system curve becomes:  $H = \left[ 0.8 * \left( \frac{Q}{Q_{100\%}} \right)^2 + 0.2 \right] * H_{100\%}$



**Issue 54:** DOE requests comment on the proposed system curve shape to use, as well as whether the curve should go through the origin instead of the statically-loaded offset.

# Efficiency of Motor and Control

- To determine the **representative** part-load losses of the motor and control, DOE analyzed the results of AHRI 1210-2011 testing for five different “motor-drive” combinations and additional, publically-available data.
  - DOE primarily considered maximum losses.
- DOE determined that **4 curves** describing combined motor + control efficiency as a function of fractional motor load and motor horsepower were the most accurate representation without being overly burdensome or complex.
  - DOE also considered curves as a function of speed, torque, motor size, and other variables.



Motor Horsepower (hp)	Coefficients for Motor and Control Part-Load Loss Factor ( $z_i$ )		
	a	b	c
≤5	-0.4658	1.4965	0.5303
>5 and ≤20	-1.3198	2.9551	0.1052
>20 and ≤50	-1.5122	3.0777	0.1847
>50	-0.8914	2.8846	0.2625

# Requests for Comment

**Issue 55:** DOE requests comment on the proposed calculation approach for determining pump shaft input power for pumps sold with motors and continuous controls when rated using the calculation-based method.

**Issue 56:** DOE requests comment on the proposal to adopt four part-load loss factor equations expressed as a function of the load on the motor (i.e., motor brake horsepower) to calculate the losses of a combined motor and continuous controls, where the four curves would correspond to different horsepower ratings of the continuous control.

**Issue 57:** DOE also requests comment on the accuracy of the proposed equation compared to one that accounts for multiple performance variables (speed and torque).

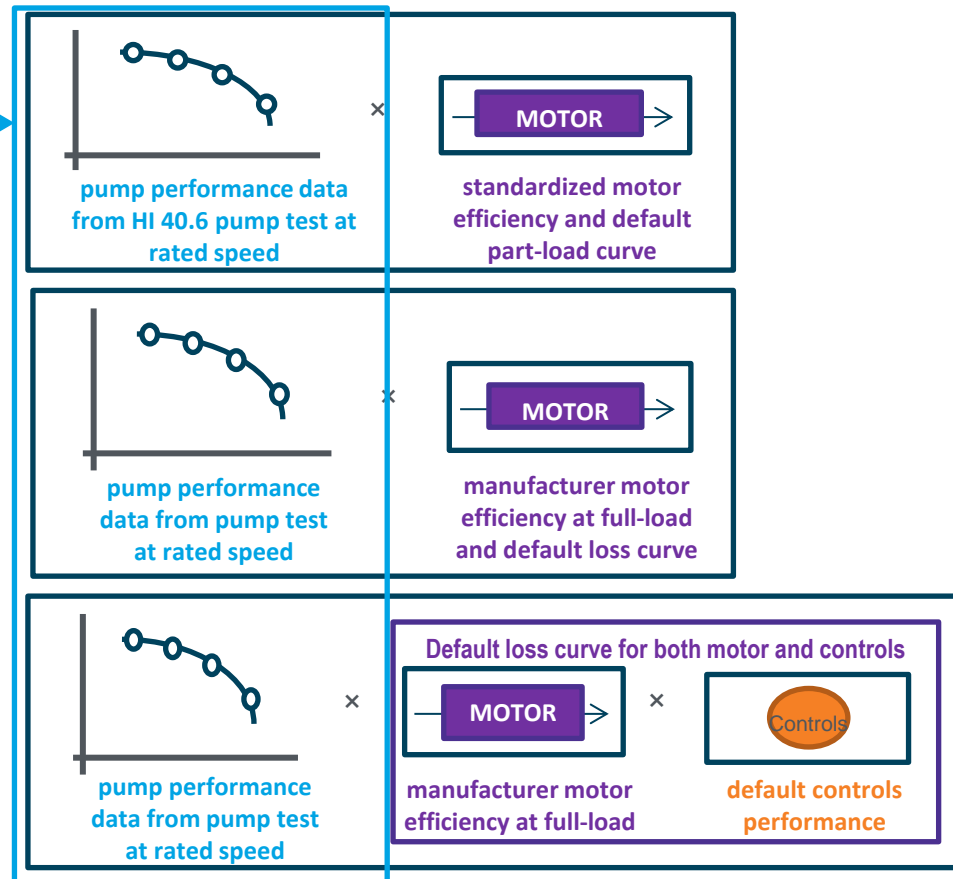
**Issue 60:** DOE requests comment and data from interested parties regarding the extent to which the assumed default part-load loss curve would represent minimum efficiency motor and continuous control combinations.

# Test of Bare Pumps and Additional Calculation Approaches

- Under the calculation-based approach, DOE proposes that testing of bare pump performance is required in all cases.

**Issue 61:** DOE requests comment on its proposal to require testing of each individual bare pump as the basis for a certified  $PEI_{CL}$  or  $PEI_{VL}$  rating for one or more pump basic models.

- DOE is not considering additional calculations or algorithms at this time.



**Issue 62:** DOE requests comment on its proposal to limit the use of calculations and algorithms in the determination of pump performance to the calculation-based methods proposed in this NOPR.

# Application of Calculation-Based Test Methods Based on Pump Configuration

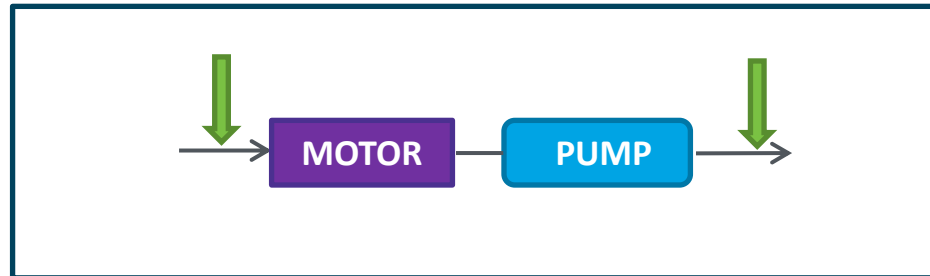
Metric	Rated As	Test Method	Applicable Pump Configurations	Calculation-Based Test Method
PEI <sub>CL</sub>	Bare Pump	Calculation-Based Only		A.1: Tested Pump Efficiency of Bare Pump + Default Motor Efficiency + Default Motor Part-Load Loss Curve
	Pump + Motor	Testing-Based Only		Not Applicable
		Testing-Based or Calculation-Based		B.1: Tested Pump Efficiency of Bare Pump + Motor Nameplate Efficiency for Actual Motor Paired with Pump + Default Motor Part-Load Loss Curve
PEI <sub>VL</sub>	Pump + Motor + Controls	Testing-Based Only		Not Applicable
		Testing-Based or Calculation-Based		C.1: Tested Pump Efficiency of Bare Pump + Motor Nameplate Efficiency for Actual Motor Paired with Pump (or Default Submersible Motor Efficiency+ Default Motor/Control Part-Load Loss Curve + Refined System Curve

# Testing Methods: Calculation- and Testing-Based

- DOE considered both testing-based and calculation-based methods for determining the metric for a given pump configuration

Test Method	Pros	Cons
Calculation-Based Approach	Repeatable; Less Burdensome	Assumptions Regarding Change in Motor/Controls Efficiency with Changing Load Required; Decreased Accuracy
Physical Testing-Based Approach	Accurate; Differentiates Performance of Different Motor/Controls Equipment at Full and Part-Load	Burdensome; Drive Test Data Not Available

# Testing-Based: B.2 – Pump Sold With a Motor



- For pumps sold with motors, the  $PEI_{CL}$  can be determined by wire-to-water testing, as specified in HI 40.6–2014 section 40.6.4.4.
  - Test similar to bare pump test, except in this case, the input power to the motor is measured directly at 75, 100, and 110 percent of BEP flow and
  - The BEP is determined based on overall efficiency  $\longrightarrow \eta_{overall} = \frac{P_{Hydro}}{P_i^{in}}$

$$PER_{CL} = \omega_{75\%}(P_{75\%}^{in}) + \omega_{100\%}(P_{100\%}^{in}) + \omega_{110\%}(P_{110\%}^{in})$$

Where:

$\omega_i$  = weighting at each rating point (equal weighting or  $1/3$  in this case),

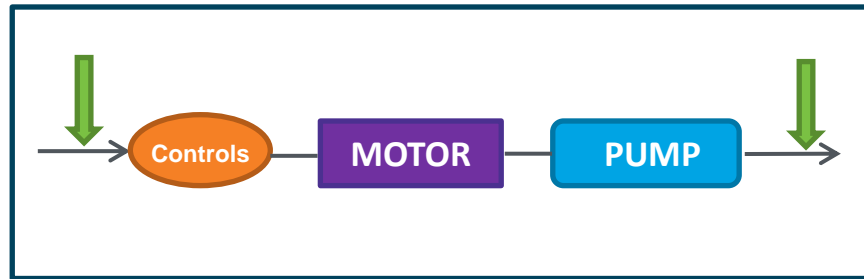
$P_i^{in}$  = measured input power to the motor at rating point  $i$ , and

$i$  = 75, 100, and 110 percent of BEP flow as determined in accordance with the DOE test procedure.

$$PEI_{CL} = \left[ \frac{PER_{CL}}{PER_{STD}} \right]$$



# Testing-Based: C.2 – Pump, Motor & Control



- For pumps sold with motors and continuous or non-continuous controls, DOE proposes that the  $PEI_{VL}$  may be determined by wire-to-water testing.
  - First, determine the BEP of the pump, inclusive of motor and continuous or non-continuous controls, at nominal speed based on overall efficiency.
  - Then adjust the operating speed of the motor and the head until the head and flow conditions specified by the reference system curve are reached.

$$PER_{VL} = \omega_{25\%}(P_{25\%}^{in}) + \omega_{50\%}(P_{50\%}^{in}) + \omega_{75\%}(P_{75\%}^{in}) + \omega_{100\%}(P_{100\%}^{in})$$

Where:

$\omega_i$  = weighting at each rating point (equal weighting or  $1/4$  in this case),

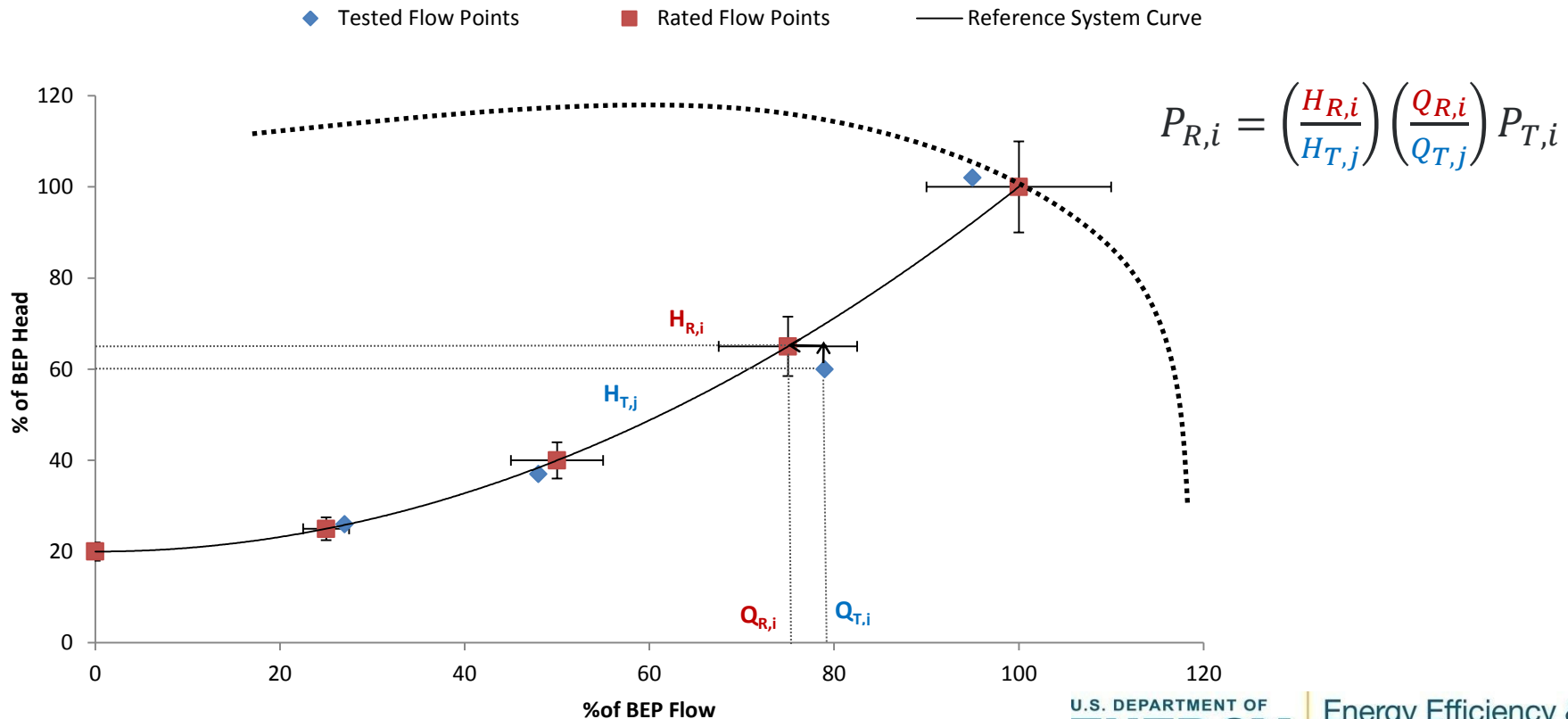
$P_i^{in}$  = **measured** input power to the controls at rating point  $i$ , and

$i$  = 25, 50, 75, and 100 percent of BEP flow as determined in accordance with the DOE test procedure.

$$PEI_{VL} = \left[ \frac{PER_{VL}}{PER_{STD}} \right]$$

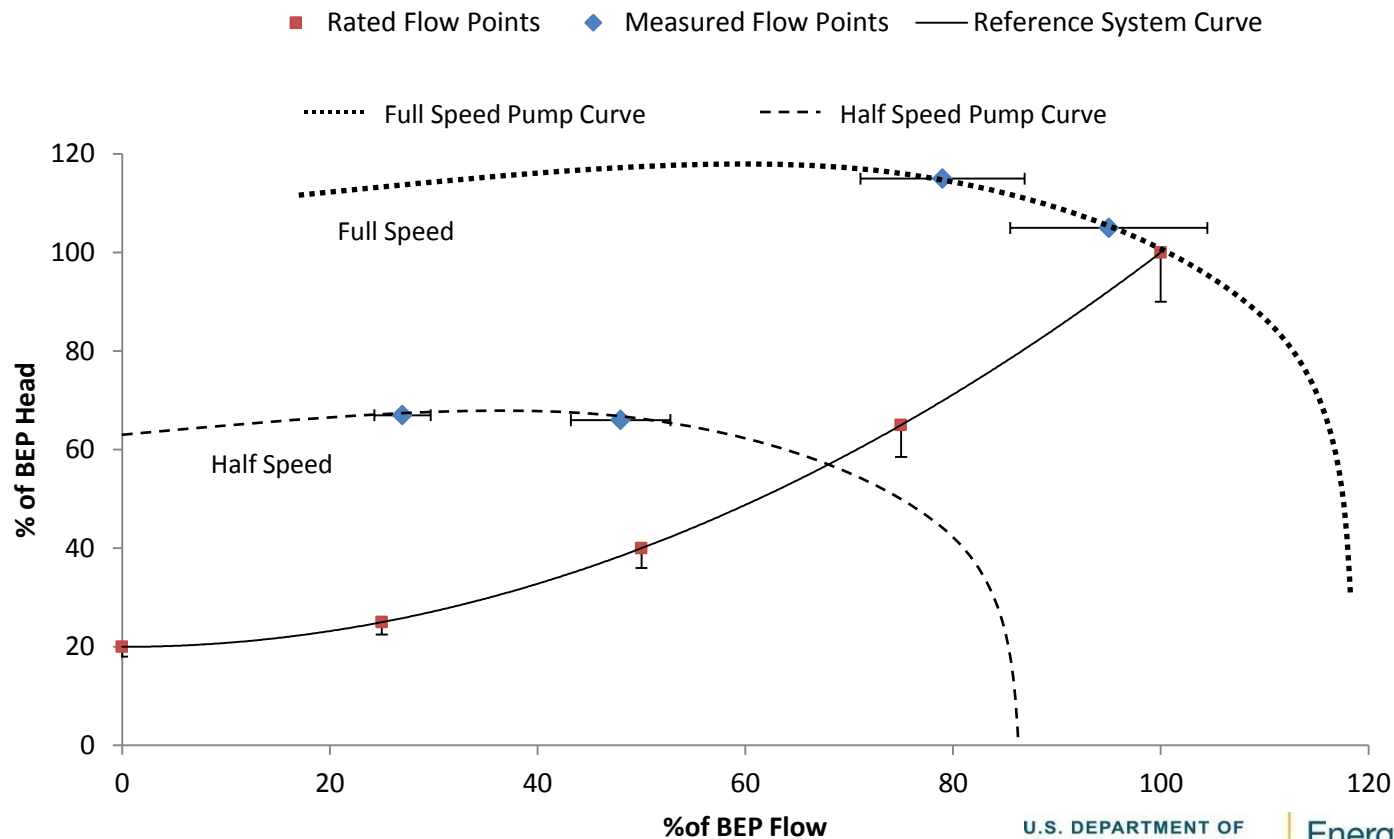
# Testing-Based: C.2 – Determining Rated Power

- To ensure accurate and consistent results, DOE is proposing:
  - that tested flow points are within 10 percent of the target flow and head load points defined on the reference system curve and
  - measured input power to the pump (at the controls) is extrapolated to the exact load points specified by the system curve.



# Test Based: C.2 – Non-Continuous Control

- In the case of non-continuous controls, the test procedure is the same as for pumps sold with motors and continuous controls (C.2), except:
  - the measured head must be no lower than 10 percent below the load points specified by the reference system curve and
  - head values above the reference system curve must be used directly and not corrected.



# Requests for Comment

**Issue 64:** DOE requests comment on the proposed testing-based method for pumps sold with motors and continuous or non-continuous controls.

**Issue 65:** DOE requests comment on the proposed testing-based method for determining the input power to the pump for pumps sold with motors and non-continuous controls.

**Issue 66:** DOE requests comment on any other type of non-continuous control that may be sold with a pump and for which the proposed test procedure would not apply.

# Application of Testing-Based Test Methods Based on Pump Configuration

Metric	Rated As	Test Method	Applicable Pump Configurations	Physical Testing-Based Test Method
PEI <sub>CL</sub>	Bare Pump	Calculation-Based Only		Not Applicable
	Pump + Motor	Testing-Based Only		B.2: Tested Wire-to-Water Performance
		Testing-Based or Calculation-Based		B.2: Tested Wire-to-Water Performance
PEI <sub>VL</sub>	Pump + Motor + Controls	Testing-Based Only		C.2: Tested Wire-to-Water Performance
		Testing-Based or Calculation-Based		C.2: Tested Wire-to-Water Performance

# Applicable Test Methods Based on Pump Configuration

Metric	Rated As	Test Method	Applicable Pump Configurations	Calculation-Based Test Method	Physical Testing-Based Test Method
PEI <sub>CL</sub>	Bare Pump	Calculate Only	Bare Pump; Pump Sold with Non-Electric Driver; Pump Sold with Single-Phase Induction Motor	A.1: Tested Pump Efficiency of Bare Pump + Default Motor Efficiency + Default Motor Part-Load Loss Curve	Not Applicable
	Pump + Motor	Testing Only	Pump + Non-Covered Poly-Phase Electric Motor (with or without Controls Other than Continuous or Non-Continuous Controls)	Not Applicable	B.2: Tested Wire-to-Water Performance
		Test or Calculate	Pump + Covered Poly-Phase Electric Motor (with or without Controls Other than Continuous or Non-Continuous Controls) OR Pump + Submersible Motor (with or without Controls Other than Continuous or Non-Continuous Controls)	B.1: Tested Pump Efficiency of Bare Pump + Motor Nameplate Efficiency for Actual Motor Paired with Pump + Default Motor Part-Load Loss Curve	B.2: Tested Wire-to-Water Performance
PEI <sub>VL</sub>	Pump + Motor + Controls	Testing Only	Pump + Non-Covered Poly-Phase Electric Motor with Continuous or Non-Continuous Controls; Pump + Covered Poly-Phase Electric Motor with Non-Continuous Controls; OR Pump + Submersible Motor with Non-Continuous Controls	Not Applicable	C.2: Tested Wire-to-Water Performance
		Test or Calculate	Pump + Covered Poly-Phase Electric Motor with Continuous Controls OR Pump + Submersible Motor with Continuous Controls	C.1: Tested Pump Efficiency of Bare Pump + Motor Nameplate Efficiency for Actual Motor Paired with Pump + Default Motor/Control Part-Load Loss Curve + Assumed System Curve	C.2: Tested Wire-to-Water Performance

# Requests for Comment

**Issue 67:** DOE requests comment on its proposal to establish (1) calculation-based test methods as the required test method for bare pumps and (2) testing-based methods as the required test method for pumps sold with motors that are not regulated by DOE's electric motor energy conservation standards, except for submersible motors, or for pumps sold with any motors and with non-continuous controls.

**Issue 68:** DOE also requests comment on the proposal to allow either testing-based methods or calculation-based methods to be used to rate pumps sold with continuous control-equipped motors that are either (1) regulated by DOE's electric motor standards or (2) submersible motors.

**Issue 69:** DOE requests comment on the level of burden that would accompany any certification requirements related to reporting the test method used by a manufacturer to certify a given pump basic model as compliant with any applicable energy conservation standard DOE may set.

# Representations of Energy Use and Energy Efficiency

- The DOE test procedure describes methods for determining  $PEI_{CL}$ ,  $PER_{CL}$ ,  $PEI_{VL}$ , and  $PER_{VL}$ .
- DOE does not wish to limit the representations manufacturers may make regarding other pump performance metrics.

Metric	Permitted Representations
<b>PEI</b>	Full Impeller Only (at Specified Number of Stages)
<b>PER</b>	Full Impeller Only (at Specified Number of Stages)
<b>Pump Efficiency, Overall Efficiency, Bowl Efficiency</b>	Multiple Impeller Trims, Operating Speeds, and Number of Stages for a Given Pump
<b>Pump Input Power, Hydraulic Output Power, and/or Brake Horsepower</b>	Multiple Impeller Trims, Operating Speeds, and Number of Stages for a Given Pump
<b>Non-Energy = Head, Flow (Especially BEP Flow), Specific Speed</b>	Multiple Impeller Trims, Operating Speeds, and Number of Stages for a Given Pump



# Public Meeting Slides Topics – Morning (TP)

- 1 Introductions & Stakeholder Opening Statements
- 2 Regulatory History & Scope
- 3 Metric
- 4 Test Procedure: Determination of Pump Performance
- 5 Break
- 6 Test Procedure: Determination of Driver Efficiency
- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Sampling Plans for Pumps

- DOE provides sampling plans in subpart B to 10 CFR part 429 for all covered equipment.
- The purpose of these sampling plans is to provide uniform statistical methods for determining compliance with prescribed energy conservation standards and when making representations of energy consumption and energy efficiency for each covered equipment type on labels and in other locations such as marketing materials.
- DOE proposes to adopt the same statistical sampling procedures that are applicable to many other types of commercial and industrial equipment in a new section (10 CFR 429.59).
  - DOE proposes to apply the minimum requirement of two tested units to certify a basic model as compliant.
  - DOE proposes to determine compliance in an enforcement matter based on the arithmetic mean of a sample not to exceed four units.

# Determining Sample Size

- Manufacturers must determine the certified rating based on the testing of a **randomly selected sample of sufficient size** such that:

- The  $PEI_{CL}$  or  $PEI_{VL}$  shall be **greater than or equal to** the higher of:

- (A) The mean of the sample:

$$\bar{x} = \frac{1}{n} \sum_{i=1}^n x_i$$

where  $\bar{x}$  is the sample mean;  $n$  is the number of samples; and  $x_i$  is the maximum of the  $i^{\text{th}}$  sample;

**Or,**

- (B) The upper 95 percent confidence limit (UCL) of the true mean divided by 1.10:

$$UCL = \bar{x} + t_{0.95} \left( \frac{s}{\sqrt{n}} \right)$$

where  $s$  is the sample standard deviation;  $n$  is the number of samples; and  $t_{0.95}$  is the  $t$  statistic for a 95 percent one-tailed confidence interval with  $n-1$  degrees of freedom.

- To pass, the certified rating determined based on the above method must be less than the standard (1.0).

**Issue 70:** DOE requests comment on the proposed sampling plan for certification of commercial and industrial pump models.

# Public Meeting Slides Topics – Morning (TP)

- 1 Introductions & Stakeholder Opening Statements
- 2 Regulatory History & Scope
- 3 Metric
- 4 Test Procedure: Determination of Pump Performance
- 5 Break
- 6 Test Procedure: Determination of Driver Efficiency
- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Review Under the Regulatory Flexibility Act

- DOE conducted a Regulatory Flexibility Act analysis for the proposed test procedure rule pursuant to the Regulatory Flexibility Act, as amended. (5 U.S.C 601, et seq.)

Initial Regulatory Flexibility Analyses	Key Assumptions	Key Findings
Identification of small businesses	<ul style="list-style-type: none"> <li>NAICS 333911, “Pump and Pumping Equipment Manufacturing,” and SBA standard ≤500 employees (13 CFR part 121) are applicable to this industry</li> </ul>	25 domestic small businesses
Assessing number of basic models	<ul style="list-style-type: none"> <li>In most cases manufacturers could use calculation-based method and, thus, burden is primarily associated with number of bare pump models</li> </ul>	Average of 41 basic models per company
Burden of conducting the test procedure	<p>Accounts for:</p> <ul style="list-style-type: none"> <li>capital expenses associated with construction and maintenance of a test facilities capable of testing pumps in compliance with the test procedure and</li> <li>recurring burden associated with ongoing testing activities (testing of 2 units per pump model)</li> </ul>	<ul style="list-style-type: none"> <li>\$61,000-\$221,000 per year per small manufacturer</li> <li>0.36-2.55% of annual sales</li> </ul>

**Issue 82:** DOE requests comment on the assumptions and estimates made in the burden analysis associated with implementing the proposed DOE test procedure.

# Public Meeting Slides Topics

- 1 Introductions
- 2 Stakeholder Opening Statements
- 3 Regulatory History & Scope
- 4 Metric
- 5 Test Procedure: Determination of Pump Performance
- 6 Test Procedure: Determination of Driver Efficiency
- 7 Test Procedure: Calculation & Testing Based Methods
- 8 Test Procedure: Sampling Plan
- 9 Test Procedure: Burden
- 10 Lunch Break

# Public Meeting Slides Topics - Standards

- 1 Overview
- 2 Market & Technology; Screening;
- 3 Engineering;
- 4 Markups Analysis; Energy Use
- 5 Life-Cycle Cost & Payback Period Analysis;
- 6 Shipments; National Impact Analysis;
- 7 MIA; NOPR Analyses; Closing Remarks
- 8 Proposed Standards; Labeling and Certification; Closing Remarks

# Regulatory History: Pumps Working Group

- The Pumps Working Group concluded on June 19, 2014, with 14 recommendations for DOE related to pump energy conservation standards and the pump test procedure (Working Group Recommendations).
- DOE's proposed energy conservation standards directly reflect the Working Group Recommendations.
- DOE conducted analysis during the Pumps Working Group to ensure that the recommended standards also meet the relevant statutory requirements.

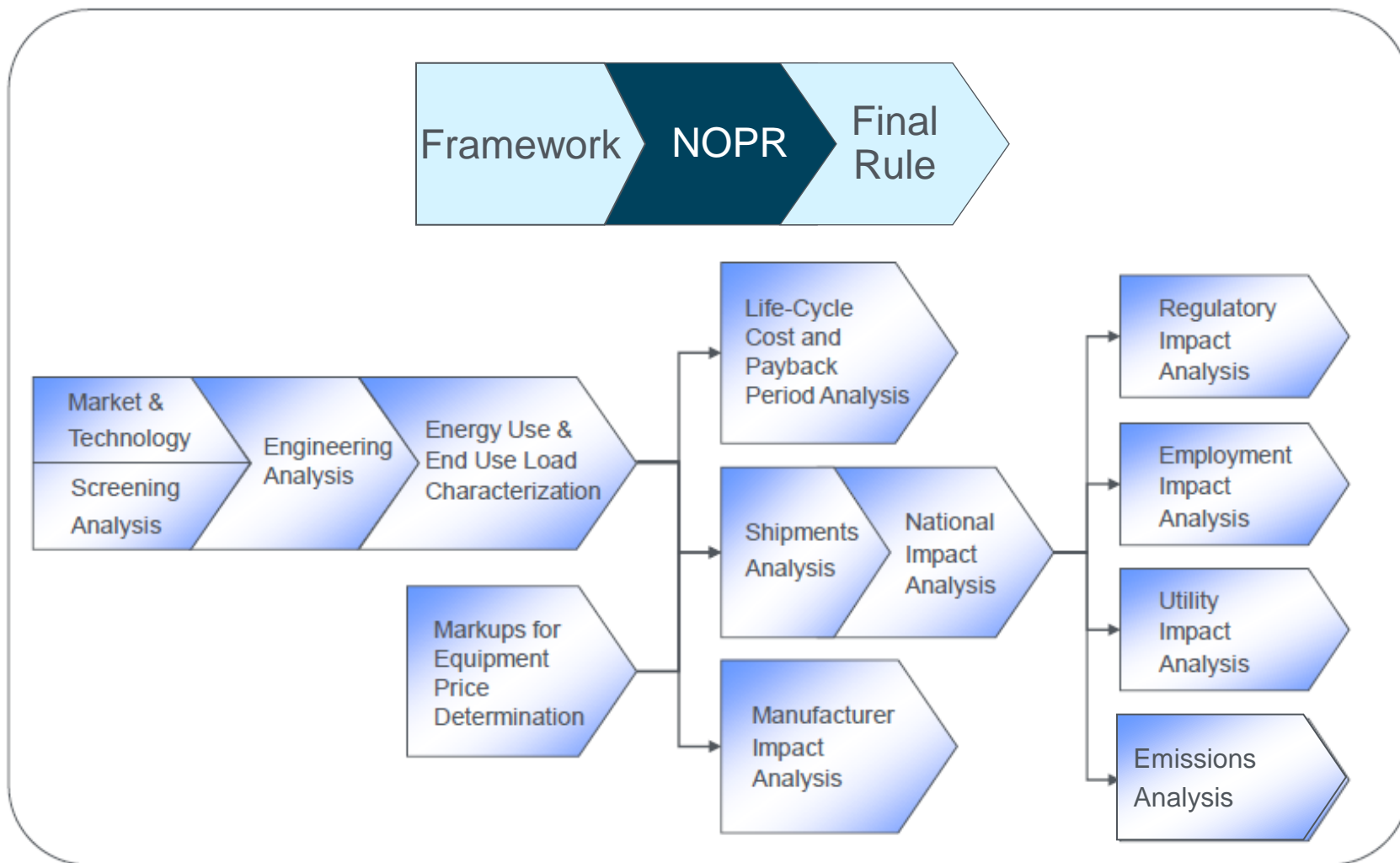


# Statutory Requirements

- Pursuant to EPCA, any new or amended energy conservation standard must be designed to achieve maximum improvement in energy efficiency that is technologically feasible and economically justified (42 U.S.C. 6295(o)(2)(A) and 6316(a), and must result in a significant conservation of energy (42 U.S.C. 6295(o)(3)(B) and 6316(a).
- EPCA also directs DOE to consider seven factors when setting energy conservation standards. (42 U.S.C. 6313(a)(6)(B))

EPCA Factors	Corresponding DOE Analyses
1. Economic impact on consumers and manufacturers	Life-Cycle Cost Analysis Manufacturer Impact Analysis
2. Lifetime operating cost savings compared to increased cost for the equipment	Life-Cycle Cost Analysis
3. Total projected energy savings	National Impact Analysis
4. Impact on utility or performance	Engineering Analysis Screening Analysis
5. Impact of any lessening of competition	Manufacturer Impact Analysis
6. Need for national energy conservation	National Impact Analysis
7. Other factors the Secretary considers relevant	Emissions Analysis Utility Impact Analysis Employment Impact Analysis

# Energy Conservation Standards Rulemaking Process



# PER<sub>STD</sub>: Minimally Compliant Pump

- The actual standard for all equipment classes and efficiency levels considered:

$$PEI = \frac{PER}{PER_{STD}} \leq 1.00$$

- The C-value in  $PER_{STD}$  varies by equipment class and with each efficiency level/trial standard level.

$$PER_{STD} = \omega_{75\%} \left( \frac{P_{Hydro,75\%}}{0.95 * \eta_{pump,STD}} + L_{75\%} \right) + \omega_{BEP} \left( \frac{P_{Hydro,100\%}}{\eta_{pump,STD}} + L_{100\%} \right) + \omega_{110\%} \left( \frac{P_{Hydro,110\%}}{0.985 * \eta_{pump,STD}} + L_{110\%} \right)$$

Determined for each pump in the test procedure

$$\eta_{pump,STD} = -0.85 * \ln(Q_{100\%})^2 - 0.38 * \ln(Ns) * \ln(Q_{100\%}) - 11.48 * \ln(Ns)^2 + 17.80 * \ln(Q_{100\%}) + 179.80 * \ln(Ns) - (C + 555.6)$$

This value changes with efficiency level to increase the efficiency of a minimally-compliant pump

# Public Meeting Slides Topics

1

Overview;

2

Market & Technology; Screening;

3

Engineering;

4

Markups Analysis; Energy Use;

5

Life-Cycle Cost & Payback Period Analysis;

6

Shipments; National Impact Analysis;

7

MIA; NOPR Analyses; Closing Remarks

8

Proposed Standards; Labeling and Certification;  
Closing Remarks

# Market and Technology Assessment

## Purpose:

- Develop the scope of coverage for this rulemaking
  - Equivalent to the scope proposed for the Test Procedure
- Define equipment classes
- Characterize the pump manufacturing industry
- Gather historical shipments and other relevant market data
- Characterize the efficiency distribution of the current market
- Identify existing regulatory and voluntary efficiency programs
- Identify technology options for improving efficiency

Note: A detailed description of methodology and results is contained in chapter 3 of the NOPR technical support document (TSD).

# Equipment Classes

DOE proposed the following 20 pump equipment classes:

Category	Sale Configuration	Design Speed (rpm)	Designation
ESCC	bare pump <u>or</u> pump with motor without controls	1800	ESCC.1800.CL
		3600	ESCC.3600.CL
	pump with motor and with controls	1800	ESCC.1800.VL
		3600	ESCC.3600.VL
ESFM	bare pump <u>or</u> pump with motor without controls	1800	ESFM.1800.CL
		3600	ESFM.3600.CL
	pump with motor and with controls	1800	ESFM.1800.VL
		3600	ESFM.3600.VL
IL	bare pump <u>or</u> pump with motor without controls	1800	IL.1800.CL
		3600	IL.3600.CL
	pump with motor and with controls	1800	IL.1800.VL
		3600	IL.3600.VL
RSV	bare pump <u>or</u> pump with motor without controls	1800	RSV.1800.CL
		3600	RSV.3600.CL
	pump with motor and with controls	1800	RSV.1800.VL
		3600	RSV.3600.VL
VTS	bare pump <u>or</u> pump with motor without controls	1800	VTS.1800.CL
		3600	VTS.3600.CL
	pump with motor and with controls	1800	VTS.1800.VL
		3600	VTS.3600.VL

# Technology Assessment

**Method:** DOE identified technology options for improved energy efficiency from publically available literature, comments and input from stakeholders, and manufacturer interviews.

**Results:** DOE identified the following technology options:

- Improved surface finish on wetted components
- Reduced running clearances
- Reduced mechanical friction in seals
- Reduction of other volumetric losses
- Improved hydraulic design
- Addition of a variable speed drive (VSD)
- Improvement of VSD efficiency
- Reduced VSD standby and off mode power usage

Note: Chapter 3 of the NOPR TSD contains a detailed description of the identified technologies.

# Screening Analysis

**Purpose:** Screen out technologies that do not save energy and/or do not meet all of the following four criteria:

1. Technological feasibility
2. Practicability to manufacture, install and service on a commercial scale at the time that compliance with any final standards would be required
3. Impacts on product utility or available to consumers
4. Impact on health and safety

**Results:**

Technology Option	Status
Reduced Running Clearances	Screened Out
Reduction of Other Volumetric Losses	Screened Out
Improved Surface Finish of Wetted Components	Screened Out
Reduced Mechanical Friction in Seals	Screened Out
Addition of a Variable Speed Drive	Screened Out
Improvement of VSD Efficiency	Screened Out
Reduced VSD Standby and Off Mode Power Usage	Screened Out
Hydraulic Redesign	Passed to Engineering

Note: Chapter 4 of the NOPR TSD discusses screening and elimination of certain technologies.



# Public Meeting Slides Topics

- 1 Overview
- 2 Market & Technology; Screening;
- 3 Engineering;
- 4 Markups Analysis; Energy Use;
- 5 Life-Cycle Cost & Payback Period Analysis;
- 6 Shipments; National Impact Analysis;
- 7 MIA; NOPR Analyses; Closing Remarks
- 8 Proposed Standards; Labeling and Certification; Closing Remarks

# Engineering Analysis

**Purpose:** Establish efficiency levels and determine incremental changes in manufacturer selling price (MSP) at each level.

## **Method:**

- Efficiency levels established using a market-distribution approach. Levels based on the current market-available range of efficiency.
- Base-case and incremental MSPs were determined using confidential market-wide revenues, shipments, and markups data, as well as specific manufacturer input.

Note: Chapter 5 of the NOPR TSD contains a detailed description of the Engineering Analysis.

# Engineering Analysis: Efficiency Levels

## Results: Efficiency Levels and Corresponding C-values

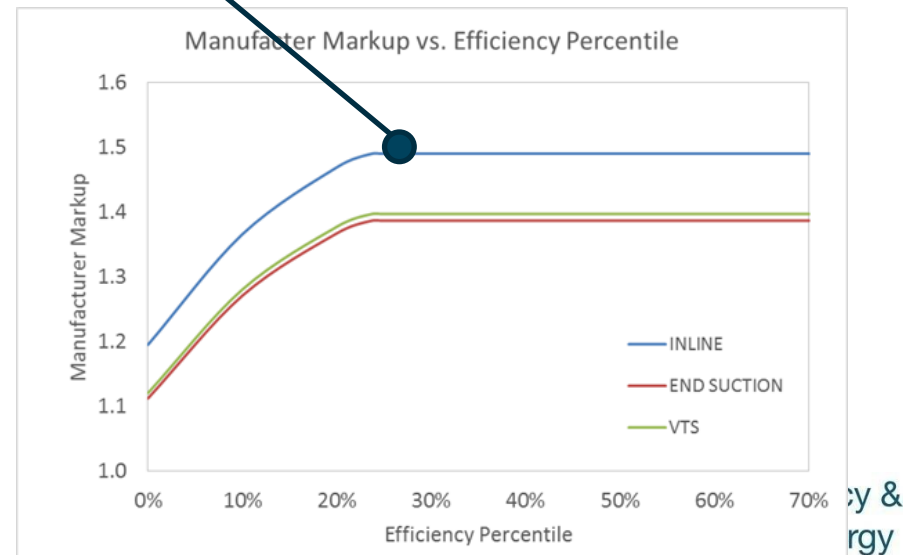
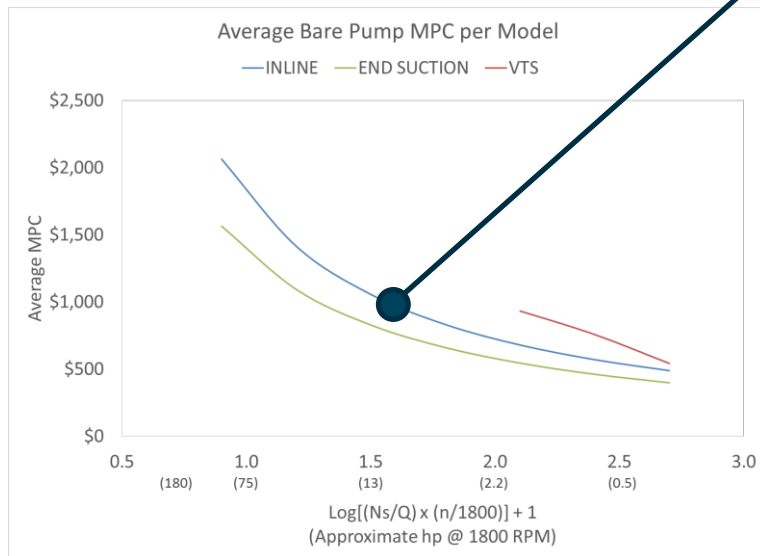
	<b>ELO</b>	<b>EL1</b>	<b>EL 2</b>	<b>EL 3</b>	<b>EL 4</b>	<b>EL 5</b>
<b>Equipment Class</b>	Baseline	10 <sup>th</sup> Efficiency Percentile	25 <sup>th</sup> Efficiency Percentile	40 <sup>th</sup> Efficiency Percentile	55 <sup>th</sup> Efficiency Percentile	70 <sup>th</sup> Efficiency Percentile/ Max Tech
<b>ESCC.1800</b>	134.43	131.63	128.47	126.67	125.07	123.71
<b>ESCC.3600</b>	135.94	134.60	130.42	128.92	127.35	125.29
<b>ESFM.1800</b>	134.99	132.95	128.85	127.04	125.12	123.71
<b>ESFM.3600</b>	136.59	134.98	130.99	129.26	127.77	126.07
<b>IL.1800</b>	135.92	133.95	129.30	127.30	126.00	124.45
<b>IL.3600</b>	141.01	138.86	133.84	131.04	129.38	127.35
<b>RSV.1800</b>	129.63	N/A	N/A	N/A	N/A	124.73
<b>RSV.3600</b>	133.20	N/A	N/A	N/A	N/A	129.10
<b>VTS.1800</b>	137.62	135.93	134.13	130.83	128.92	127.29
<b>VTS.3600</b>	137.62	135.93	134.13	130.83	128.92	127.29

# Engineering Analysis: Base-Case MSP-Efficiency Relationship

## Results: Base-Case MSP-Efficiency Relationship

- DOE found a relationship between manufacturer markup and efficiency.
- DOE determined that improved efficiency does not increase manufacturer production cost (MPC).
- DOE modeled the average MPC for pumps within scope.
- The base-case MSP for a pump of a given size and efficiency (MSP-Efficiency Relationship) is found using the Average MPC Model (below, left) and the Markup vs. Efficiency Percentile model (below, right) for each equipment class:

$$MSP = MPC \times Markup$$



# Engineering Analysis: Conversion Costs

Hydraulic redesigns result in significant conversion costs and manufacturers may use increased markups to recover these conversation costs.

**Method:** Bottom-up approach to find industry conversion costs

1. Determine the industry-average cost, per model, to redesign pumps of varying sizes to meet each of the proposed efficiency levels.
2. Model the distribution of unique pump models that would require redesign at each efficiency level.
3. For each efficiency level, multiply the number of unique failing models by the associated cost to redesign and sum to reach an estimate of the total conversion cost for the industry.

## Results:

Aggregate Industry Conversion Cost at Each Efficiency Level (Million USD)						
All Values in Millions of Dollars	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	Baseline	10 <sup>th</sup> Percentile	25 <sup>th</sup> Percentile	40 <sup>th</sup> Percentile	55 <sup>th</sup> Percentile	70 <sup>th</sup> Percentile
ESCC/ESFM*	\$0	\$12.4	\$49.4	\$110.6	\$210.4	\$344.7
IL	\$0	\$5.1	\$20.0	\$45.3	\$88.2	\$144.0
VTS	\$0	\$2.5	\$9.3	\$19.2	\$37.8	\$61.3
<b>Total Industry</b>	\$0	\$20.0	\$78.7	\$175.1	\$336.4	\$550.0

Note: Chapter 5 of the NOPR TSD contains a detailed description of the Conversion Cost Analysis.

# Engineering Analysis: Standards-Case MSP-Efficiency Relationship

**Method:** DOE evaluated two standards-case MSP-Efficiency scenarios to represent the uncertainty regarding the potential impacts of standards on prices and profitability.

## 1. Flat Pricing

- Pricing structure not modified to recover conversion costs.
  - *i.e.*, Same markup structure as in the base-case
- This scenario is considered a lower bound for revenues.

## 2. Cost Recovery Pricing

- Pricing structure modified to recover conversion costs over the analysis period.
  - *i.e.*, Increased markups, even as MPC remains the same
- This scenario is considered an upper bound for revenues.
- This scenario provides the highest cost to consumers and is used for the LCC analysis.

**Results** are incorporated into the LCC and MIA analyses

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# Markups Analysis

## Purpose

- Determine consumer prices based on manufacturer's selling price for baseline and higher efficiency equipment
- Characterize pump distribution channels

## Method

- Analyze company direct costs, expenses, and profits
  - Original Equipment Manufacturers: U.S. Census Bureau, *2007 Manufacturing Industry Series*
  - Distributors: U.S. Census Bureau, *2012 Annual Wholesale Trade Survey, Hardware, Plumbing, and Heating Equipment and Supplies Merchant Wholesalers*
  - Contractors: RSMeans, *2013 Electrical Cost Data*
  - Sales Taxes: *The Sales Tax Clearinghouse, 2014*
- Calculate baseline and incremental markups
  - Baseline markups applied to MSP of baseline level
  - Incremental markups applied to incremental difference in MSP at each level above baseline; covers only expenses that vary with MSP, or in this case, expense that increase due to an efficiency standard



# Markups Analysis: Overall Markups

Markup	Manufacturer to Distributor to Contractor to End-User (70%)		Manufacturer to Distributor to End-User (17%)		Manufacturer to OEM to End-User (8%)		Manufacturer to End-User (2%)		Manufacturer to Contractor to End-User (1%)		Other (2%)	
	Base-line	Incr.	Base-line	Incr.	Base-line	Incr.	Base-line	Incr.	Base-line	Incr.	Base-line	Incr.
<b>OEM</b>	-	-	-	-	1.43	1.38	-	-	-	-	-	-
<b>Distributor</b>	1.39	1.15	1.39	1.15	-	-	-	-	-	-	-	-
<b>Contractor</b>	1.1	1.1	-	-	-	-	-	-	1.1	1.1	-	-
<b>Sales Tax</b>	1.07	1.07	1.07	1.07	1.07	1.07	1.07	1.07	1.07	1.07	-	-
<b>Overall</b>	<b>1.64</b>	<b>1.35</b>	<b>1.49</b>	<b>1.23</b>	<b>1.53</b>	<b>1.48</b>	<b>1.07</b>	<b>1.07</b>	<b>1.18</b>	<b>1.18</b>	<b>1.59</b>	<b>1.34</b>

- NOTE: These markups are applied to the MSP, which already includes the manufacturer markup.

# Energy Use Analysis

## Purpose

- Determine annual energy use (UEC) of pumps at the considered efficiency levels to find annual energy costs and savings.
- Annual energy costs are inputs to Life-Cycle Cost and Payback Period Analysis.

## Method

- The annual energy use is calculated as a weighted sum of input power multiplied by the annual operating hours across all load points.

$$AEU = \sum_{\text{LoadProfile}} \frac{Q_i \times H_i}{\eta_i \eta_{motor,i}} \times OpHour_i$$

– where:

- $Q_i$  is the flow load point
- $H_i$  is the head at  $Q_i$ , calculated from the pump curve
- $\eta_i$  is the pump efficiency calculated from the efficiency curve
- $\eta_{motor,i}$  is the motor efficiency
- $OpHour_i$  refers to annual hours of operation at load point  $i$

# Energy Use Analysis: Inputs

Input	Description
<b>Duty Point</b>	The LCC uses a set of representative units constructed from binning the manufacturer survey data into 9 power bins x 9 flow bins, logarithmically spaced. All efficiencies within a bin are assumed available for the representative unit. Pump curve, efficiency curve, base price and BEP efficiency are normalized to the bin average specific speed and flow.
<b>Pump Sizing</b>	Represented by a “BEP offset:” $Flow_{Duty} = (1 + x)Flow_{BEP}$ X is chosen from a uniform distribution between -0.25 to 0.10 (to represent pump sizing between 75% and 110% of BEP flow).
<b>Annual Hours of Operation</b>	Distributions of annual operating hours by application based on a consultant estimate with Pumps Working Group review and modification.
<b>Load Profile</b>	4 typical load profiles – flat load [30%], flat/over-sized [30%], variable/over-sized [30%], and variable/under-sized [10%].
<b>Pump Losses</b>	Accounted for using efficiency curve calculated for each representative unit.
<b>Motor Losses</b>	Selected a motor using the default sizing procedure in the TP NOPR (based on power required at 120% BEP flow). For each motor pole and horsepower configuration, used the minimum motor efficiency values under 10 CFR 431.25. Determined part-load motor losses using default method in the TP NOPR.
<b>Control Losses</b>	Assumed that all users with variable loads were throttling their pumps. VSD users handled in a sub-group analysis.

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# Life-Cycle Cost (LCC) and Payback Period (PBP) Analysis

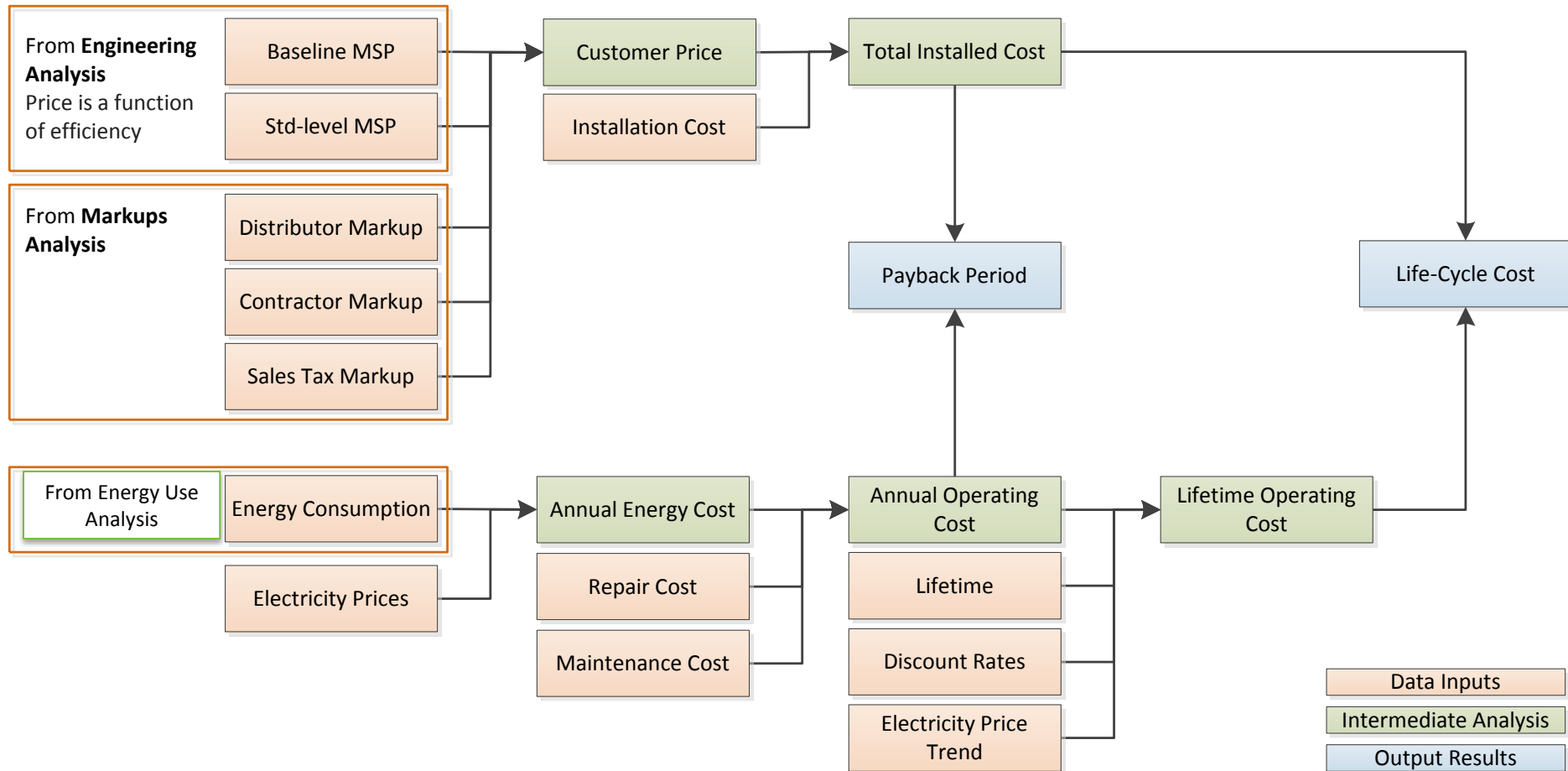
## Purpose

- Provide an economic evaluation from the consumer's perspective.
- Life-Cycle Cost (LCC) is the total consumer cost over the life of the equipment.
- Payback Period (PBP) is the time required to recover the increased purchase price of more energy-efficient equipment through reduced operating costs.

## Method

- 10,000 pump installations (pump user + pump) for each LCC run.
- Many variables (discount rate, operating hours per year, total lifetime operating hours, load profile type) are chosen from distributions.
- User characteristics (including lifetime and operating hours) are the same for all efficiency levels.
- In the base case, pumps are distributed to users according to the efficiency distribution in the shipments.
- Pump characteristics change with EL if the user's base case pump does not pass the efficiency criteria for that EL.
- If a pump fails, a user purchases the same pump that has been redesigned to meet the efficiency level in each standards case.

# LCC and PBP Analysis: Overview



# LCC and PBP Analysis: Inputs

Input	Description
Sample Weights	Fraction of total sample by pump type, speed, power, flow, sector, and application determined based on databases of pump operation in the field, consultant estimates, and shipment data.
Equipment Price	In the base case, determined from the MSP (engineering analysis) and distribution channel markups (markups analysis). In each standards case, new MSPs for redesigned pumps are determined by distributing conversion costs (engineering analysis) to each power and flow bin based on percentage of total revenue, and dividing the new revenue requirement by the number of failing pumps. Constant real prices used to project pump equipment prices. (PPI does not show a clear trend after 2009.)
Installation Cost	Not expected to change with efficiency level, so not included in analysis.
Annual Energy Use	Provided by the Energy Use Analysis.
Electricity Prices	Based on average national commercial and industrial electricity prices from the <i>AEO 2014</i> reference case, with extrapolation after 2040.
Maintenance Cost	Not expected to change with efficiency level, so not included in analysis.
Repair Cost	Not expected to change with efficiency level, so not included in analysis.
Equipment Lifetime	Started with typical service lifetimes in years. Used a distribution of mechanical lifetime in hours to allow a negative correlation between annual operating hours and lifetime in years. Also lifetime variation by pump speed.
Discount Rate	Used to convert streams of annual operating expenses to the year of purchase (i.e., 2020). For industrial, commercial, and agricultural, estimated using the CAPM model (equity capital) and Damodaran Online (debt financing). For municipal, calculated based on inflation-adjusted interest rates on state and local bonds from 1983 to 2012, issued by the Federal Reserve.
Efficiency Distribution	Determined by performance data of shipments provided by manufacturers and HI.

# LCC and PBP Analysis: ESCC 3600 Results

Efficiency Level	Average Costs (2013\$)				Average Savings (2013\$)	Percent of Consumers with Net Cost (%)	Simple Payback (years)
	Installed Cost	First Year's Operating Cost	Lifetime Operating Cost	LCC			
Base Case	1,092	1,592	9,823	10,915	-	-	-
EL 1	1,098	1,588	9,800	10,898	17	1	1.4
EL 2	1,111	1,574	9,713	10,823	92	2	1.0
EL 3	1,141	1,565	9,653	10,794	122	14	1.8
EL 4	1,170	1,551	9,566	10,736	180	14	1.9
EL 5	1,215	1,528	9,422	10,638	278	12	1.9



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# Shipments Analysis

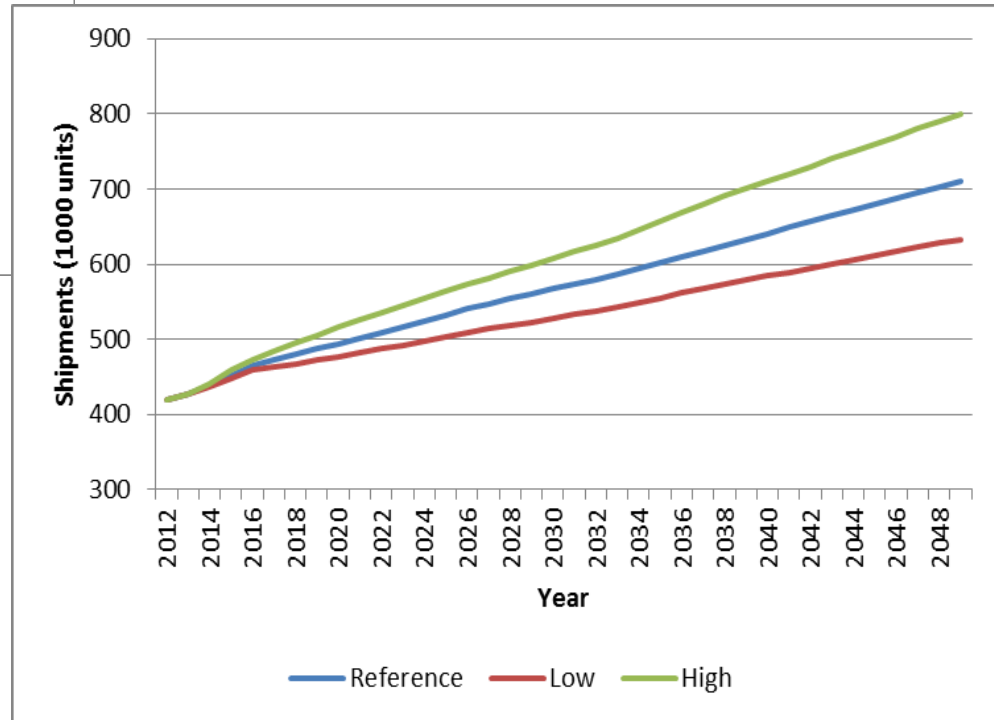
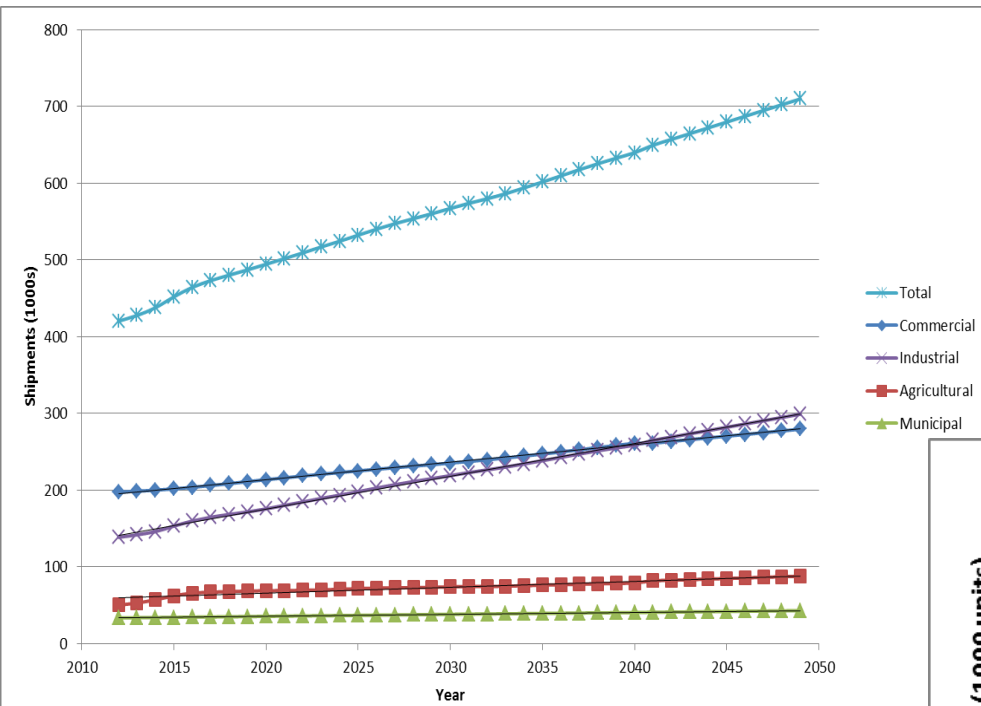
## Purpose

- To estimate shipments over the 30-year analysis period.
- Shipments are inputs to the National Impact Analysis.

## Method

- Use initial shipments estimates for each equipment class from the Hydraulic Institute and major manufacturers.
- Distribute total shipments into four sectors using estimates from the LCC.
- Project shipments by sector using the application of indicator variables from *AEO 2014* forecasts:
  - (1) commercial floor space,
  - (2) value of manufacturing shipments (industrial),
  - (3) value of agriculture, mining, and construction shipments (ag), and
  - (4) population (municipal).
- Disaggregate into equipment class based on 2012 market shares.
- Use same shipments in base case and standards case.

# Shipments Analysis: Results



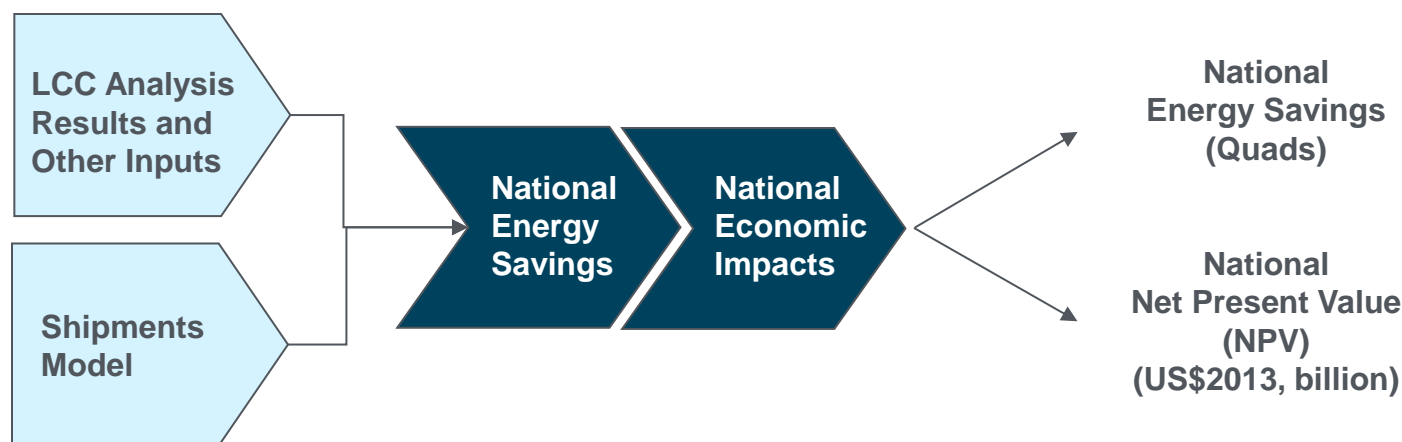
# National Impact Analysis

## Purpose

- Determine the projected national energy savings and consumer national net present value.

## Method

- Develop annual series of national energy and economic impacts.
- Use the shipments model to estimate the total stock of pumps in service each year.
- Calculate National Energy Savings for 30 years of shipments (2020-2049) as the difference between standards case cumulative energy use and base case cumulative energy use.
- Calculate NPV for 30 years of shipments (2020-2049) by comparing standards case to base case in terms of cumulative operating cost savings (energy costs) and cumulative installed cost increases (equipment prices) and applying a discount rate.



# National Impact Analysis: Inputs

Input	Description
<b>Total Installed Cost</b>	Weighted-average per unit values as a function of efficiency level taken from the LCC analysis. Equipment costs vary with efficiency level. Because installation costs do not vary by efficiency level, they are not included in this analysis.
<b>Repair and Maintenance Costs</b>	Maintenance and repair costs do not vary as a function of efficiency level, and are not included in this analysis.
<b>Annual Energy Use</b>	Annual weighted-average per unit values as a function of efficiency level taken from LCC analysis. Additional adjustments made for trimmed impellers and pumps used with VFDs, which may reduce potential energy savings.
<b>Base-Case Efficiencies</b>	Shipments-weighted efficiencies determined for the compliance year. Based on base-case efficiency distribution from LCC analysis. No projected growth.
<b>Standards-Case Projected Efficiencies</b>	For each efficiency level analyzed, DOE used a “roll-up” scenario to establish the market shares by efficiency level. No change in efficiency distribution over time.
<b>Energy Prices</b>	Projected energy prices from EIA <i>AEO 2014</i> forecasts (to 2040) and extrapolated thereafter.
<b>Full-Fuel-Cycle</b>	Multiplier to convert site energy to full-fuel-cycle energy.
<b>Discount Rate</b>	7 percent and 3 percent real from OMB’s Regulatory Analysis Guideline A-4.
<b>Present Year</b>	Future expenses are discounted to the year 2015.

# National Impact Analysis: Trial Standard Levels

TSL	Formulation Criteria
1	Each equipment class (except RSV) moves up one efficiency level from the current baseline; RSV remains at baseline.
2	Each equipment class (except RSV) moves up two efficiency levels from the current baseline; RSV remains at baseline.
3	Each equipment class (except RSV) moves up three efficiency levels from the current baseline; RSV remains at baseline.
4	Each equipment class (except RSV) moves up four efficiency levels from the current baseline; RSV remains at baseline.
5	Maximum technologically feasible level, maximum NPV and maximum NES. Each equipment class (except RSV) moves up five efficiency levels from the current baseline. RSV moves to max-tech.

# National Impact Analysis: Trial Standard Levels

Equipment Class	Baseline	TSL 1	TSL 2	TSL 3	TSL 4	TSL 5
	Efficiency Level/C-value					
ESCC 1800	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	134.43	131.63	128.47	126.67	125.07	123.71
ESCC 3600	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	135.94	134.60	130.42	128.92	127.35	125.29
ESFM 1800	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	134.99	132.95	128.85	127.04	125.12	123.71
ESFM 3600	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	136.59	134.98	130.99	129.26	127.77	126.07
IL 1800	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	135.92	133.95	129.30	127.30	126.00	124.45
IL 3600	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	141.01	138.86	133.84	131.04	129.38	127.35
RSV 1800*	EL 0	EL 0	EL 0	EL 0	EL 0	EL 5
	129.63	129.63	129.63	129.63	129.63	124.73
RSV 3600*	EL 0	EL 0	EL 0	EL 0	EL 0	EL 5
	133.20	133.20	133.20	133.20	133.20	129.10
VTS 1800*	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	137.62	135.93	134.13	130.83	128.92	127.29
VTS 3600	EL 0	EL 1	EL 2	EL 3	EL 4	EL 5
	137.62	135.93	134.13	130.83	128.92	127.29

127 \*Equipment classes not analyzed due to lack of available data (RSV) or lack of market share (VT-S 1800)

# National Impact Analysis: National Energy Savings

## Cumulative Full-Fuel-Cycle National Energy Savings

Equipment Class	TSL 1	TSL 2	TSL 3	TSL 4	TSL 5
	quads				
<b>ESCC 1800</b>	0.017	0.05	0.08	0.12	0.17
<b>ESCC 3600</b>	0.017	0.08	0.12	0.18	0.28
<b>ESFM 1800</b>	0.003	0.06	0.12	0.25	0.37
<b>ESFM 3600</b>	0.002	0.02	0.03	0.05	0.07
<b>IL 1800</b>	0.016	0.05	0.08	0.12	0.17
<b>IL 3600</b>	0.003	0.01	0.02	0.02	0.03
<b>VTS 3600</b>	0.002	0.02	0.11	0.17	0.24
<b>TOTAL</b>	0.059	0.28	0.56	0.91	1.32

Note: Components may not sum to total due to rounding.



# National Impact Analysis: Consumer NPV

## National Net Present Value

Equipment Class	Discount Rate	TSL 1	TSL 2	TSL 3	TSL 4	TSL 5
		Billion 2013\$				
ESCC 1800	3%	0.052	0.20	0.29	0.40	0.47
	7%	0.018	0.07	0.11	0.14	0.15
ESCC 3600	3%	0.069	0.34	0.46	0.68	1.06
	7%	0.028	0.14	0.18	0.26	0.41
ESFM 1800	3%	0.010	0.20	0.44	0.88	1.28
	7%	0.003	0.06	0.14	0.27	0.39
ESFM 3600	3%	0.009	0.08	0.14	0.20	0.30
	7%	0.003	0.03	0.05	0.07	0.11
IL 1800	3%	0.063	0.18	0.25	0.28	0.34
	7%	0.022	0.06	0.08	0.07	0.07
IL 3600	3%	0.011	0.04	0.06	0.08	0.11
	7%	0.004	0.01	0.02	0.03	0.04
VTS 3600	3%	(0.001)	0.07	0.49	0.71	0.90
	7%	(0.002)	0.02	0.20	0.28	0.35
TOTAL	3%	0.213	1.11	2.13	3.23	4.47
	7%	0.077	0.41	0.77	1.13	1.51

\*Numbers in parenthesis indicate negative NPV

Note: Components may not sum to total due to rounding.

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Closing Remarks

# MIA: Overview

## Purpose:

- To assess the impacts of standards on manufacturers
- To identify and estimate impacts on manufacturer subgroups that may be more severely affected than the industry as a whole
- To examine the direct employment, manufacturing capacity, and cumulative regulatory impacts on the industry

## Methodology:

- Analyze industry cash flow and industry net present value (INPV) using the Government Regulatory Impact Model (GRIM):
- Interview manufacturers to refine inputs to the GRIM, develop subgroup analyses, and address qualitative issues

# MIA: INPV

## Results:

	Units	Base Case	Trial Standard Level				
			1	2	3	4	5
INPV	(2013\$ M)	121.4	111.6 to 121.8	81.9 to 129.7	22.4 to 125.4	(85.0) to 114.1	(228.4) to 94.1
Change in INPV	(%)	-	(8.0) to .3	(32.5) to 6.9	(81.6) to 3.3	(170.0) to (6.0)	(288.2) to (22.5)

# MIA: Small Business Impacts

## Results:

- DOE identified twenty-five domestic small business manufacturers of pumps falling into the classes that would be addressed by the proposed standards.
- DOE only identified one small manufacturer that exclusively produced covered product.
- In aggregate, approximately 24% of product offerings from small manufacturers were covered by this rule.
- DOE estimates the impacts of a standard on an average small business manufacturers would be comparable to the impacts on an average large manufacturer.

# NOPR Analyses

- **LCC Subgroup**
  - DOE calculated the LCC and PBP for consumers who operate their pumps with variable-frequency drives (VFD) as they will typically have lower energy use and may be disproportionately impacted compared with the general user population.
- **Emissions Impact**
  - Estimates full-fuel-cycle emissions reductions resulting from amended energy conservation standards, including carbon dioxide (CO<sub>2</sub>), sulfur dioxide (SO<sub>2</sub>), nitrogen oxides (NO<sub>x</sub>), nitrous oxide (N<sub>2</sub>O), and methane (CH<sub>4</sub>), mercury (Hg).
  - Use AEO 2014 to derive emissions factors applied to annual energy savings from NIA.
- **Emissions Monetization**
  - DOE uses the most current Social Cost of Carbon (SCC) values developed by an interagency process.
  - DOE also monetizes the NO<sub>x</sub> emissions reductions resulting from amended standards.
- **Utility Impact**
  - DOE estimates changes in electricity capacity and generation that would result from amended energy conservation standards (as compared to the base case).
  - Uses cases published from the National Energy Modeling System (NEMS) that incorporate efficiency-related policies to estimate the marginal impacts of reduced energy demand on the utility sector.
- **Employment**
  - Uses the ImSET (Impact of Sector Energy Technologies) model for the evaluation of indirect employment impacts resulting from amended energy conservation standards.
- **Regulatory Impact**
  - DOE modified the NIA spreadsheet to analyze the six non-regulatory alternatives and their impact on purchase price and energy use; presents NES and NPV for these alternatives.

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# Proposed Standard Levels

Equipment Class	Maximum PEI*	C-value**
ESCC 1800	1.00	128.47
ESCC 3600	1.00	130.42
ESFM 1800	1.00	128.85
ESFM 3600	1.00	130.99
IL 1800	1.00	129.30
IL 3600	1.00	133.84
RSV 1800	1.00	129.63
RSV 3600	1.00	133.20
VTS 1800	1.00	134.13
VTS 3600	1.00	134.13

\*Equipment rated at constant load:  $PEI_{CL}$ ; Equipment rated at variable load:  $PEI_{VL}$

\*\*C-values shown must be used in the equation for  $PER_{STD}$  when calculating  $PEI_{CL}$  or  $PEI_{VL}$ .



# Labeling Requirements

- The Pumps Working Group recommended that pumps be labeled based on the configuration in which they are sold:

Bare Pump	Bare Pump + Motor	Bare Pump + Motor + Controls
$PEI_{CL}$	$PEI_{CL}$	$PEI_{VL}$
Model number	Model number	Model number
Impeller diameter for each unit	Impeller diameter for each unit	Impeller diameter for each unit

- DOE proposes that these labeling requirements be applied to marketing materials and pump nameplates.

# Certification Requirements

- The Pumps Working Group recommended specific data be included in certification reports.
  - DOE proposes to require the data recommended by the Working Group, with additions and clarifying modifications.
- The following list summarizes selected key certification data requirements proposed by DOE:
  - Equipment class and rating configuration
  - Nominal and tested speed in rpm, at the BEP
  - BEP flow rate and head at nominal operating speed
  - Pump efficiency at BEP
  - Nominal motor hp and efficiency
  - Driver input hp at each load point, corrected to nominal speed
  - $PEI_{CL}$  or  $PEI_{VL}$ , and whether  $PEI_{CL}$  or  $PEI_{VL}$  is calculated or tested

NOTE: For the complete list of requirements see Section VI of the NOPR document.

# Pool Pumps RFI

- The Pumps Working Group recommended that dedicated-purpose pool pumps be addressed as part of a separate rulemaking. Pumps Working Group Recommendation # 5B
- On April 28, 2015, DOE issued an RFI for dedicated-purpose pool pumps that discussed the following topics:
  - Review of existing regulatory and voluntary programs
  - Scope (definitions, parameters, product type, sales configuration)
  - Test procedure and rating metrics
  - Data needs for rulemaking analysis
- To clearly distinguish dedicated-purpose pool pumps from the pumps, DOE proposed the following design-based definition:
  - **Dedicated-purpose pool pump** means an end suction pump designed specifically to circulate water in a pool and **that includes an integrated basket strainer.**
- The RFI poses whether to treat several types of pumps as dedicated-purpose pool pumps:
  - Inground and aboveground
  - Inflatable pool (integrated filter systems)
  - Auxiliary
  - Spa
  - Pool cover
  - Solar-powered and bottom-feeder

# Closing Remarks

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**Meeting participants are invited to provide any closing remarks or statements at this time.**